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Trends in the global cement industry and opportunities for long-term sustainable CCU potential for Power-to-X

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Abstract:

In order to achieve targets set by the Paris Agreement and limit global average temperature increase to well below 2 °C above pre-industrial levels, an assessment and a low carbon transformation is needed for all types of human activities. Cement production is associated with high levels of CO₂ emissions, with an average of 866 kg of CO₂ emitted per ton of cement produced. This positions the cement industry as one of the main sources of anthropogenic greenhouse gas emissions accounting for about 5% of the total, right after the chemical industry and more relevant than the iron and steel industry. About 50% of the emissions are caused by burnt fuel, related transport and other inputs, which can be currently substituted by other measures. However, the CO₂ emissions which originate from input limestone cannot be avoided. These process CO₂ emissions present a potential for carbon capture and utilisation. This research proposes a global potential analysis of CCU as a possible solution for the CO₂ emissions of cement production. Cement CCU may establish a substantial route to use CO₂ for synthetic hydrocarbons production and thus contribute towards mitigating the non-substitutable CO₂ content of the limestone-based raw material. The production of renewable electricity based synthetic hydrocarbon fuels by CO₂ captured from cement plants, counts for a potential to produce between 3639 TWh_{th} and 7355 TWh_{th} of liquid hydrocarbons, or 6298 TWh_{th} and 12723 TWh_{th} of synthetic natural gas, or a mix of both at the expected global cement peak production in 2040.

Keywords: Cement, GHG emissions, power-to-fuels, carbon capture, carbon utilisation

Nomenclature

BAU	Business as usual
BCSa	Best case scenario - alternative fuels
BCSe	Best case scenario - electric
CaCO ₃	Limestone
CaL	Calcium looping
CaO	Lime
CC	Carbon capture
CCS	Carbon capture and storage
CCU	Carbon capture and utilisation
CO ₂	Carbon dioxide
CO _{2eq}	Carbon dioxide equivalent
CSIt	Cement sustainability initiative target
DAC	Direct air capture
FLh	Full load hours
GDP	Gross domestic product
GHG	Greenhouse gases
HHV	High heating value
LCOE	Levelised cost of electricity

MENA	Middle East and North Africa
Mt	Megaton
MWh _{th}	Megawatt hour, thermal
PtG	Power-to-gas
PtL	Power-to-liquids
PtX	Power-to-X
RE	Renewable Energy
R ²	Coefficient of determination
SAARC	South Asian Association for Regional Cooperation
SNG	Synthetic natural gas
TWh _{th}	Terawatt hour, thermal
TWh _{el}	Terawatt hour, electric
WBCSD	World Business Council for Sustainable Development

Highlights

- The cement industry is responsible for up to 8% of anthropogenic CO₂ emissions.
- 50% of the CO₂ currently emitted during cement production comes from raw materials.
- The only option for partly decarbonising cement production is carbon capture.
- The captured carbon from cement processing can be used to produce synthetic fuels.
- Up to 5389 TWh_{th} of synthetic gas can be produced from non-avoidable cement-based emissions in 2050.

1. Introduction

The cement industry produces the second most consumed product by weight in the world after steel, utilising roughly 1.9% of the global electricity generation [1, 2]. Thereby releasing globally from 5% to 8% of anthropogenic CO₂ emissions [3, 4, 5, 6]. The industry uses an average global energy demand of 1.025 MWh_{th} and releases greenhouse gas (GHG) emissions of 866 kg of CO_{2eq} per metric ton (referred just as ton in the rest of the paper) of clinker, respectively [4]. Furthermore, the global cement industry has grown by a factor of 25 compared to 1950's level, increasing capacity by 73% from just 2005 to 2013 [5]. Moreover, China produced and consumed more cement between 2011 and 2013 than the United States of America in the previous 100 years [5], adding up to around 3.8 Gt of cement production and 3.2 Gt of CO_{2eq} emissions and 3.895 TWh_{th} of energy consumed in 2012 [6].

However, reducing emissions from the process of cement making is not so straight forward, since it depends on different factors. According to [4] and [7], roughly 50% of the GHG emissions from the cement manufacturing process are material-derived, 40% are fuel-derived, electricity accounts for 5% of the emissions and transport generates the residual 5%. The GHG emissions can depend on factors such as technology used, fuel type, emission control system, geographic location, and the source of electrical power [4]. Emissions from the raw material are due to the chemical composition of limestone (CaCO₃), which through thermal processing releases CO₂ to reduce the compound to lime (CaO), the core component of cement.

Figure 1 shows a simplified flow diagram of the cement manufacturing process from mining to final product. Details of the manufacturing process are provided by [8, 9]. Several stages of the cement production process can be fully decarbonised. Electricity can be produced from renewable sources [10] and carbon-neutral fuels can be generated [11] to use for the

transportation of cement and provide the required heating for thermal processing. The thermal processing can also be done by electricity [12] or direct solar energy [13] instead of fuels, but the material-derived emissions cannot be easily avoided.

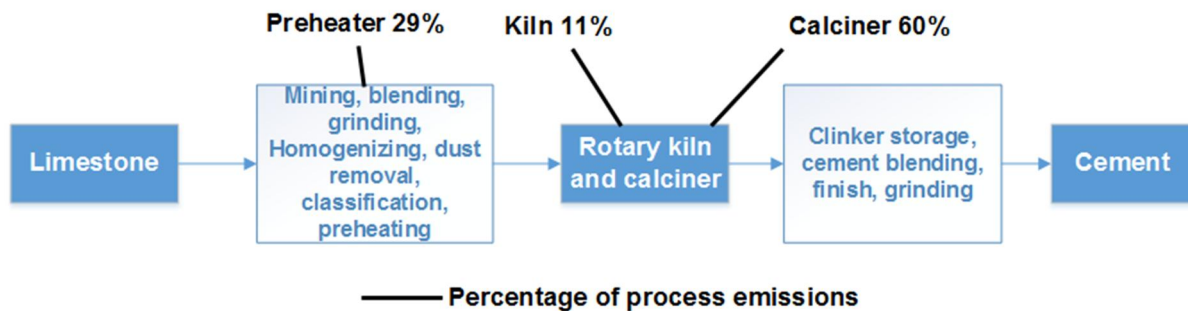


Figure 1: Simplified flow diagram of the cement manufacturing process. The percentages of process emissions are estimated and exclude the steps before preheating (mining, grinding, preheating, etc.), and after the cement production (packaging, transportation).

Nevertheless, in order to achieve the targets of the Paris Agreement [14] and prevent global average temperature to raise above 1.5 °C pre-industrial levels, it is necessary to get as close to zero GHG emissions by 2050 as possible. The power sector can be transformed to zero GHG emissions in a relatively easier manner, if strong commitments are made, as the resources and conditions are proven to exist already, and expected to further develop in the next few years [10, 15]. Whereas, cement manufacturing as it is, is incompatible with the zero emissions requirement of the near future. Limestone is considered equivalent to coal by [16], as the thermal processing of limestone releases a similar amount of CO₂ as the combustion of coal for its thermal energy. Also, both limestone and coal are carbon sources of fossil origin. Also in [16] cement is proposed, just as coal, an important candidate for carbon capture, though it is pointed out in the same study that carbon capture and storage (CCS) is not a viable strategy for cement emissions, just as it has proven to be in the case of coal-fired power plants. CCS is highly dependent of geographical and geological conditions and it would double the capital and operational costs of a cement plant [16].

Alternatives to limestone for cement production are also proposed in [16], some even with potential of negative carbon emissions. However, switching to such alternatives are still farfetched, as the properties and durability of alternative compounds are still to be tested, both in laboratories and in real life applications. Therefore, in this research yet another alternative is proposed, carbon capture and utilisation (CCU). CCU has the potential of compensating for the offset in capital and operational expenditures added by adapting carbon capture to the cement process. By utilising the captured carbon to produce synthetic (and valuable) hydrocarbon fuels or chemicals [11, 17], it is possible to compensate to some extent, both the cost of carbon capture, and also carbon emissions of the otherwise utilised fossil derived hydrocarbon fuels, at least during the transition period. One type of CCU in the case of cement and concrete that has considerable research behind is the carbonation curing of concrete masonry blocks [18-21]. These precast blocks can absorb between 17% [19] and 25% [20] of their mass in CO₂ while perceiving an increase in their compressive strength. However, precast concrete represents only 20% to 30% of the global market of concrete [20].

After the phase out of fossil fuels in the cement production process, the net GHG emissions of the cement process cannot be avoided anymore. However, it may still lower the costs of synthetic hydrocarbon production for a lower CCU cost compared to the CO₂ direct air capture

alternative. Multiple technologies have been proposed for carbon capture from the cement process. Amine scrubbing, already available for other processes shows high potential, but also new concepts such as calcium looping (CaL) could eventually prove to be advantageous alternatives. Carbon capture techniques can be further improved by oxy-combustion. A techno-economic analysis of the different technologies and their forecasted efficiencies are presented by Leeson et al. [22]. Reported efficiencies vary widely in forecasts (from 52% to 94%) even for the same analysed process (CaL), and further scepticism should be given to overly high efficiencies, taking into account that none of these technologies are yet commercially available for the cement industry. The assumed incremental efficiencies for carbon capture (expecting the process to improve over time) are 60%, 70% and 80% for 2030, 2040 and 2050 respectively, as the technology evolves [23].

2. Methodology and Data

A comprehensive list of all cement production sites, as well as their operators, capacities, and host countries were obtained from the Global Cement Directory [24], which were compared and complemented with [25], and further compiled into a database. The database on a country basis is provided in the supplementary material to this research. Furthermore, each cement manufacturing location obtained from the aforementioned sources was then localised through satellite aerial view. All of the active and registered cement factories across the world are plotted and shown in Figure 2.

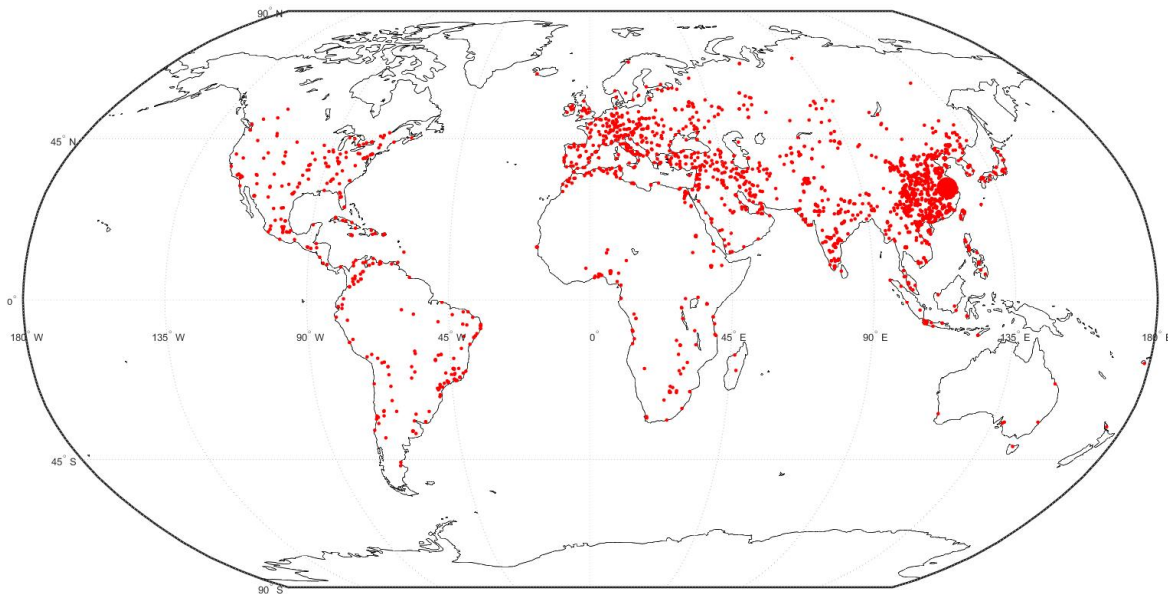


Figure 2: Global cement production sites. Larger circles represent production sites of significantly higher capacity than the others. Data are obtained from [24, 25].

In Figure 2 are plotted the over 2300 operating cement production sites from a total of over 2500 currently registered (the difference being deactivated, under construction or in planning plants). A few of them (1.3%) are capable of producing several tens of megatons (Mt) per year, some others producing just kilotons of special concretes per year, but the majority of the production sites (63% of the active cement plants) produce between 0.4 Mt to 2 Mt per year. Active cement plants by the end of 2016 registered in the database sum up to a production capacity of 3746 Mt of cement per year. It is clear from Figure 2 that the cement is produced globally, but mostly consumed locally, as limestone is a rather commonly available raw

material and the production process and machinery are simple enough to be deployed close to demand sites. Figure 3 shows how the cement plants are distributed by capacity. As it can be seen, globally 83% of the cement is produced in plants with capacities of over 1 Mt per year, and 28% is produced in plants with capacities of over 4 Mt per year.

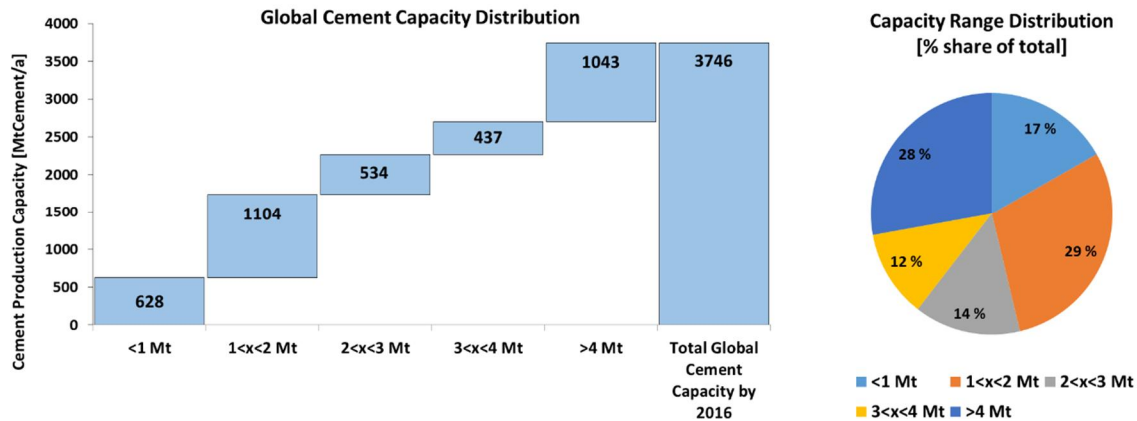


Figure 3: Distribution of installed capacities by capacity range.

Cement production, as shown in Figure 2, tends to be close to population centres, as those places represent the target consumers of the product. As it is used for housing and infrastructure such as roads, hospitals, schools, sewage, etc., which is further driven by the cost structure and the high density of cement leading to fast rising cost fractions of transportation as a function of distance. Much like population, China holds the highest capacity in a single country with 36.8% of the global cement production. Other countries with high production capacity shares of cement are India (8.7%), United States of America (3.3%), Russia (3.0%), Vietnam (2.8%), Turkey (2.6%), Brazil (2.3%) and Iran (2.3%). Together the top 10 cement producing countries hold 65.7% of the total global production.

An extract of the database and the main countries across the world in cement production capacity are presented in Table 1. The CO_{2eq} emissions are estimated based on [25] records by taking an average of the emissions per ton of cement in the past 10 years in each region, as the emissions depend to some degree on the location and quality of the raw material.

Table 1: Main countries in the cement industry globally, region distributions, and their respective estimated emissions. The capacity numbers are for end of 2016 and equivalent to a full year of production. Data are taken from Global Cement Directory [24]. The CO_{2eq} emissions estimate is based on [25].

Country	Cement Capacity [Mt/a]	CO _{2eq} emissions estimated [MtCO _{2eq} /a]
China	1367.0	1170.1
India	324.6	276.3
United States	120.8	112.4
Russia	110.8	95.2
Vietnam	105.6	89.8
Turkey	96.4	82.1
Brazil	85.5	73.4
Iran	84.7	72.1
Saudi Arabia	73.5	62.5
Indonesia	71.7	61.0

Region	Cement Capacity [Mt/a]	CO _{2eq} emissions estimated [MtCO _{2eq} /a]
Global	3713.4	3206.9
Top10	2440.6	2094.9
EU-28	275.4	236.6
Share Top 10	65.1 %	65.3 %
Share EU-28	7.3 %	7.4 %
China only	36.5 %	36.5 %

Figure 4 shows the total active production capacity installed in regions. The scale was set as logarithmic since the difference in active installed capacities has large variations from region to region, especially when compared with China.

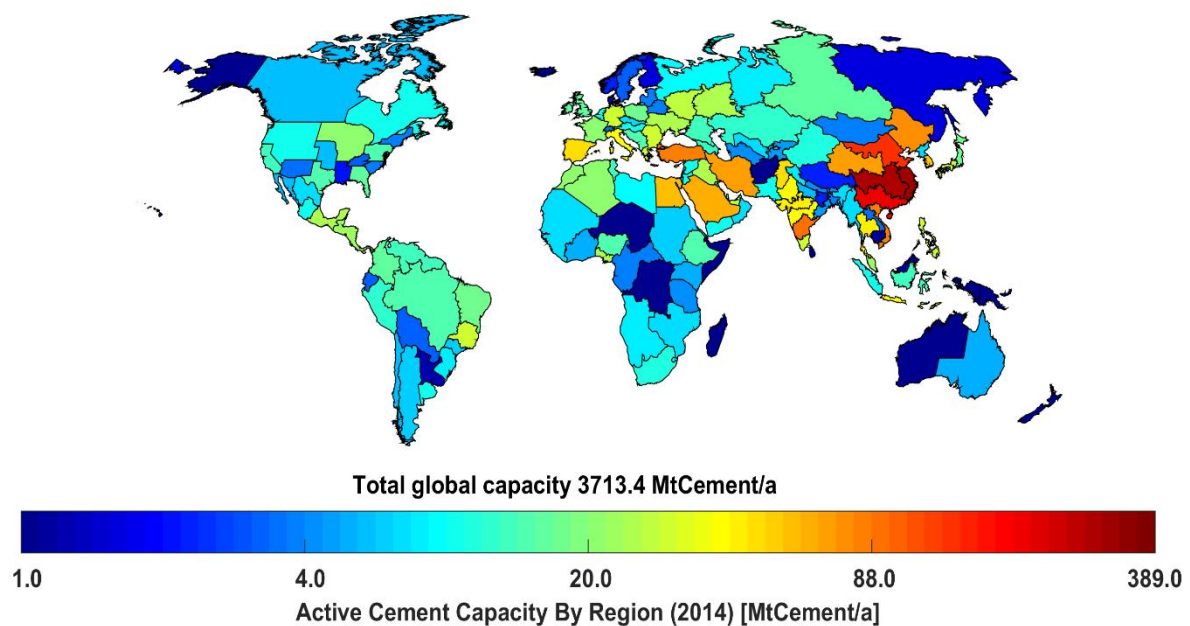


Figure 4: Global cement production capacity installations structured in regions shown in logarithmic scale.

So far, proposed roadmaps for carbon reduction as mentioned in [4, 5, 6, 17, 26, 27, 28] present de-carbonisation strategies for replacing fossil fuels with synthetic or carbon neutral ones and using RE sources, which still leaves a potential of around 1.56 Gt of GHG emissions to be tackled by 2050, while double of that is already being emitted today. Some of these strategies can (and are expected to) be implemented to reduce GHG emissions immediately, but the insufficiency of the approach to fully eliminate CO_{2eq} emissions is what sets the stage for carbon capture strategies.

Currently, the situation is as plotted in Figure 5, showing the consumption of cement per capita compared to the gross domestic product (GDP) per capita globally. The red line (generated by the function of Equation 1) represents the projected demand of cement per capita as a function of development of GDP per capita, as van Ruijven et al. [29] found a strong correlation between GDP and cement and steel usage. Intuitively, cement requirements are higher during the development phase of each country, during which roads, harbours, airports, urban areas, hospitals, schools, and many other infrastructures are built. Once developed, the demand of cement per capita drops significantly, as the requirement for new infrastructure is reduced to a minimum and cement is then utilised mostly for maintenance and replacement.

A	$4.2 \cdot 10^{-3}$
B	$-9 \cdot 10^{-5}$
C	$-4.74 \cdot 10^{-3}$
D	$-1.6 \cdot 10^{-4}$
E	$1 \cdot 10^{-6}$
F	$9 \cdot 10^{-6}$
G	$2.5 \cdot 10^{-4}$

Variable	Definition (Equation 2)
$f(x)$	Tailored fitting function for cement/GDP per capita projection
P_i	Cement production per capita of country i
K_i	Active cement production capacity of country i
Q_i	$f(x)$ value for the GDP per capita of country i
\overline{PK}	Average value of the sum from $i=1$ to n of $P_i \cdot K_i$
R^2	Coefficient of determination
n	Total number of countries

Carbon and hydrogen are the main building blocks for hydrocarbons and many other chemicals. In the power-to-gas (PtG) approach, RE is used to generate hydrogen by water electrolysis. In the next step, methane is produced synthetically from hydrogen and CO₂ by using the Sabatier reaction in a methanation unit. With CO₂ already available, the overall process can reach an efficiency of 65% based on high heating value (HHV) in 2030 [11].

In the power-to-liquids (PtL) approach, to generate longer-chained hydrocarbons, H₂ and CO₂ are first converted to a mixture of H₂ and CO (known as syngas) in a reverse water-gas shift unit. In the next step, the syngas is converted to syncrude (a mixture of different hydrocarbons such as light fuel gases, naphtha, kerosene, diesel and waxes) in a Fischer-Tropsch reactor. The heavy liquids and waxes could be broken down to lighter hydrocarbons with a shorter carbon chain in a hydrocracker unit. The system could run on diesel or kerosene mode, aiming for the highest share of each (60% diesel or 50% kerosene) in the output, according to the demand. The PtL overall efficiency could reach 54% by 2030. In addition, there would be excess heat available from both PtG and PtL processes [11]. The bulk chemicals such as methanol can be produced in different reactors under different chemical reactions [17, 30].

2.1. Power-to-X assumptions

The idea or concept of applying carbon capture to the cement manufacturing process has been analysed before. Different studies compiled by Leeson et al. [22] show a range of efficiencies and techniques for carbon capture. The two main trends are amine scrubbing and calcium looping, both supported by oxy-combustion. The level of assumptions and considerations used by each of the analysed cases is different, and so are the results, reporting for processes of oxy-combustion + CaL with efficiencies from 52% to 94%. This significant level of uncertainty and the fact that technologies proposed for carbon capture are at best in pilot stage for the cement industry complicates the selection of a specific efficiency. Instead, incremental efficiencies for carbon capture will be assumed, using 60% efficiency until 2030 and increasing to 70% and 80% for 2040 and 2050, respectively. Furthermore, taking into account that only 50% of the emissions are associated with the limestone thermal processing, rest of the emissions could be neutralised by replacing the fuel from coal and natural gas with RE-based carbon-neutral synthetic fuels, biofuels, waste, biomass or avoided by direct use of renewable electricity. The

transportation share of the emissions can be avoided by usage of electric vehicles or running combustion vehicles with synthetic fuels or biofuels.

In order to analyse the CO₂ potential for synthetic hydrocarbons four different case scenarios are defined, with the range of energy consumption presented in Table 3 and level of emissions presented in Table 4. The emission levels per ton of cement according to the different scenarios are represented in Figure 6 and the evolution of CO₂ emitted and captured as well as estimated cement production is shown in Figure 7. The efficiencies of carbon capture (excluding transportation emissions) are 60% for the calculations before 2030, and 70% and 80% for the years 2040 and 2050, respectively. The four scenarios represent very distinct pathways, so that individual pathways can be created as a mix of the presented scenarios to also reflect different diffusion dynamics of new technologies and measures, which can be varied on a per country basis with the data provided in the Supplementary Material. The scenarios are as follows:

- *Business as usual (BAU)*: Continuation with the current trends of coal and natural gas for fuel with a 10% share of alternative fuels (waste and biomass) at a global average, with considering the specific average CO₂ emissions of every region per ton of clinker before carbon capture, according to the World Business Council for Sustainable Development (WBCSD) database [25].
- *Cement sustainability initiative target (CSIt)*: WBCSD [25] target for CO₂ emissions reduction, at -18.7% of BAU CO₂ emissions per ton of clinker (-24% net CO₂ emissions) before carbon capture. This is achieved through higher shares (up to 37%) of alternative fuels utilised (assuming the CO₂ fuel emissions presented by [31] and the waste emissions measured by [32]), and improving technology efficiency.
- *Best case scenario - alternative fuels (BCSa)*: CO₂ emissions reduction of -42.9% of BAU per ton of clinker due to use of oxy-fuel combustion with 50% hydrogen (rounded as the share of hydrogen used in [33] and 50% waste as fuel for thermal processing of limestone. Emissions from electricity and transportation are excluded, as they cannot be captured, but in principle could already be neutralised (e.g. through renewable energy and use of electric vehicles). It is assumed that this scenario can be achieved from 2030 onwards. The technology improvements of the CSIt scenario are also assumed.
- *Best case scenario - electric (BCSe)*: Emissions reduction of -50% of BAU per ton of clinker by using electricity from RE sources, and transportation emissions are neglected as in the previous scenario. Use of electricity derived from renewable sources is assumed to be used for the thermal processing of limestone [12] (with only the emissions of the raw material remaining). It is assumed that this scenario can be achieved from 2030 onwards and technology improvements of the CSIt scenario are applied. This scenario may exhibit the highest engineering challenges among the four scenarios as the process itself would change substantially, and there is not yet technology available at the commercial stage. Therefore, the assumption on energy consumption is estimated as in BCSa and CSIt, though when developed and implemented for industrial scale the technology may show different consumption.

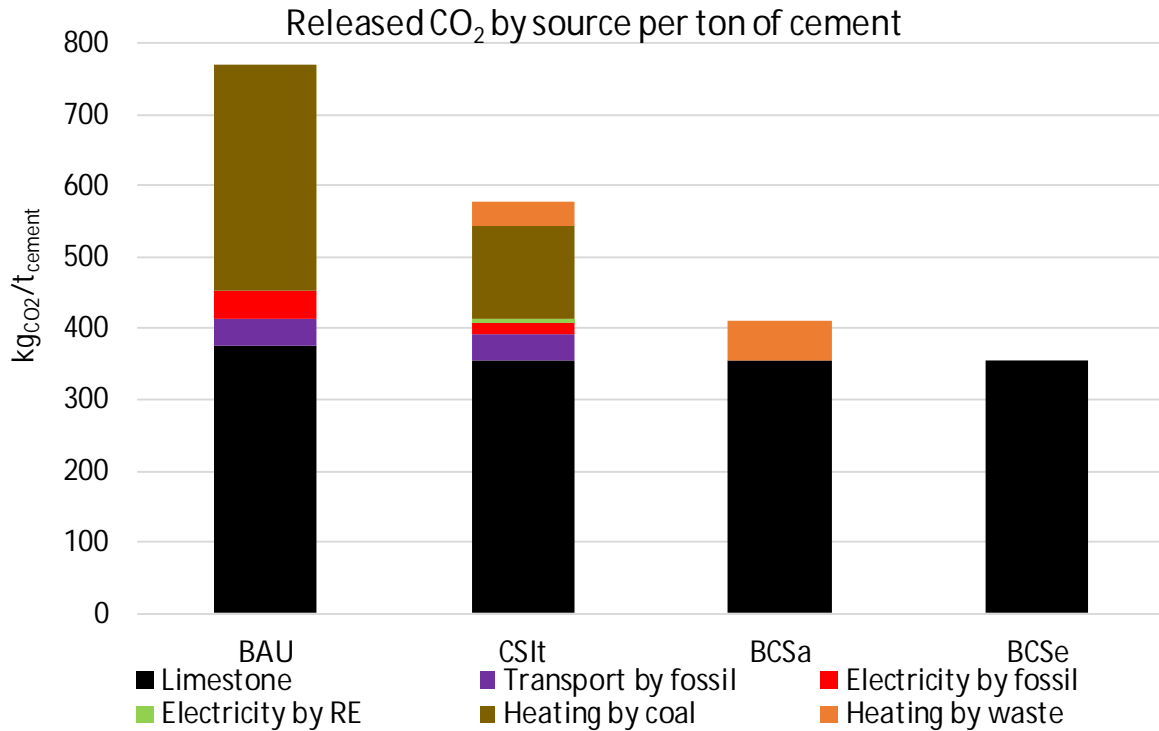


Figure 6: Emission levels by source for different scenarios.

Table 3: Estimated range of energy demand for different scenarios. Mean electricity demand for BAU is taken from [34] and range of electricity demand is taken from [35]. Range of heat energy for BAU is taken from [4]. The following ranges are assumed with the mean values between the average in BAU and the minimum for BAU, with BCSe having the most uncertainty.

Scenario	Min Heat Energy	Mean Heat Energy	Max Heat Energy	Min Electric Energy	Mean Electric Energy	Max Electric Energy
BAU	707 kWh	919 kWh	1616 kWh	70 kWh	106 kWh	140 kWh
CSIt	707 kWh	813 kWh	919 kWh	70 kWh	88 kWh	106 kWh
BCSa	707 kWh	813 kWh	919 kWh	70 kWh	88 kWh	106 kWh
BCSe	707 kWh	813 kWh	919 kWh	70 kWh	88 kWh	106 kWh

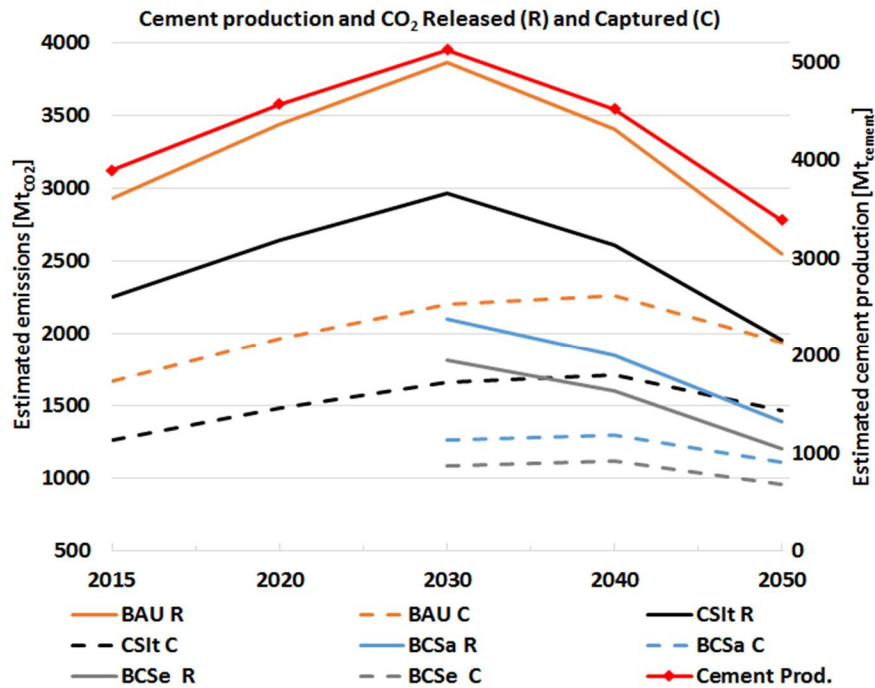


Figure 7: Timeline estimation of total global cement production (red), as well as CO₂ released (R) in solid lines and captured (C) in dashed lines respectively for every scenario.

Table 4: Estimated cement production, CO₂ emissions and captured CO₂ potential for the different defined scenarios. The assumptions for the potential for the captured CO₂ are 60% for the years before 2030, and 70% and 80% for 2040 and 2050 respectively in all scenarios, and -6% clinker to cement ratio for CSIt and both BCS scenarios.

Total estimated emissions before carbon capture [MtCO ₂]					
	Cement production estimated [Mt]	BAU	CSIt	BCSa	BCSe
2015	3896	2934	2252	n/a	n/a
2020	4569	3441	2640	n/a	n/a
2030	5124	3859	2961	2098	1814
2040	4517	3401	2610	1849	1599
2050	3387	2551	1957	1387	1199

Total estimated captured CO ₂ potential for Power-to-X usage [MtCO ₂]						
	Cement production estimated [Mt]	BAU	CSIt	BCSa	BCSe	Assumed CO ₂ capture efficiency
2015	3896	1672	1263	n/a	n/a	60%
2020	4569	1961	1481	n/a	n/a	60%
2030	5124	2199	1661	1259	1088	60%
2040	4517	2262	1708	1294	1119	70%
2050	3387	1938	1464	1109	959	80%

Considering the previously mentioned available CO₂, two options are proposed for Power-to-X (PtX): synthetic natural gas (SNG) production through Power-to-Gas (PtG) and synthetic liquid hydrocarbons through Power-to-Liquids (PtL). The CO₂ would be provided by carbon

capture technologies. The two leading technologies for carbon capture are calcium looping (CaL) and amine scrubbing [36], both fairly well developed for application in energy conversion systems.

CaL consists of two interconnected fluidised bed reactors, of which in the first (carbonation reactor) flue gas is treated with a calcium-based sorbent (which can be lime itself from the cement processing cycle) at temperatures in the range of 650-850°C and atmospheric pressure [37]. The formed particles of CaCO₃ are then separated and sent to the second reactor (calcination reactor), an oxy-fired fluidised bed at over 900°C that produces a close-to-pure CO₂ suitable for storage and lime (CaO) for recycling into the carbonator [36, 37]. Over several cycles, the lime loses reactivity and it becomes part of the clinker output, while new limestone for processing can refresh the reactive lime into the reaction. The main advantage of this technology is that flue gases can be treated at a high temperature and low pressure that is already produced from the cement processing process. However, there is still no research on how the unreactive lime affects the characteristics of the clinker or cement, and how it limits the capacity of concrete to later absorb CO₂.

Amine scrubbing, which is widely used in the chemical sector [36, 37], consists of chemical gas-liquid absorption using alkanolamines. The flue gas is cooled down and then treated by exposing it to contact with an amine liquid solution in the absorption stack. Afterwards, the CO₂-rich solvent is transferred to another stack where it is treated with heat for desorption, separating the CO₂ for condensing and storage, and the solvent for recycling back to the absorption column [36]. One of the main disadvantages of amine scrubbing is the need for cooling of the flue gasses before the treating and the additional heating required for the desorption process. It should be noted that, though both carbon capture techniques are fairly developed, they are not efficiently coupled to the cement processing system because of the differences of the cement processing in comparison with other point source carbon emitters, such as power plants.

3. Results

3.1. Current state

As shown in Figure 5, China is positioned at the peak of the projection function. Even though the Chinese production and demand from 2010 to 2013 was still increasing dramatically, in the past few years it has halted and even decreased, due to basic infrastructure being mostly deployed, resulting in under-utilisation and over-capacities [38]. Though the world's main producing and consuming country seems to have already peaked, still a large number of countries remain in the underdeveloped zone of less than 10,000 €per capita, which means that the global cement production is expected to grow. At the same time some Middle Eastern countries such as Saudi Arabia, Qatar, Kuwait, Oman, etc. show an “inflated” consumption of cement, mostly because of the instantly generated wealth from the oil and gas industry boom in a previously heavily underdeveloped area.

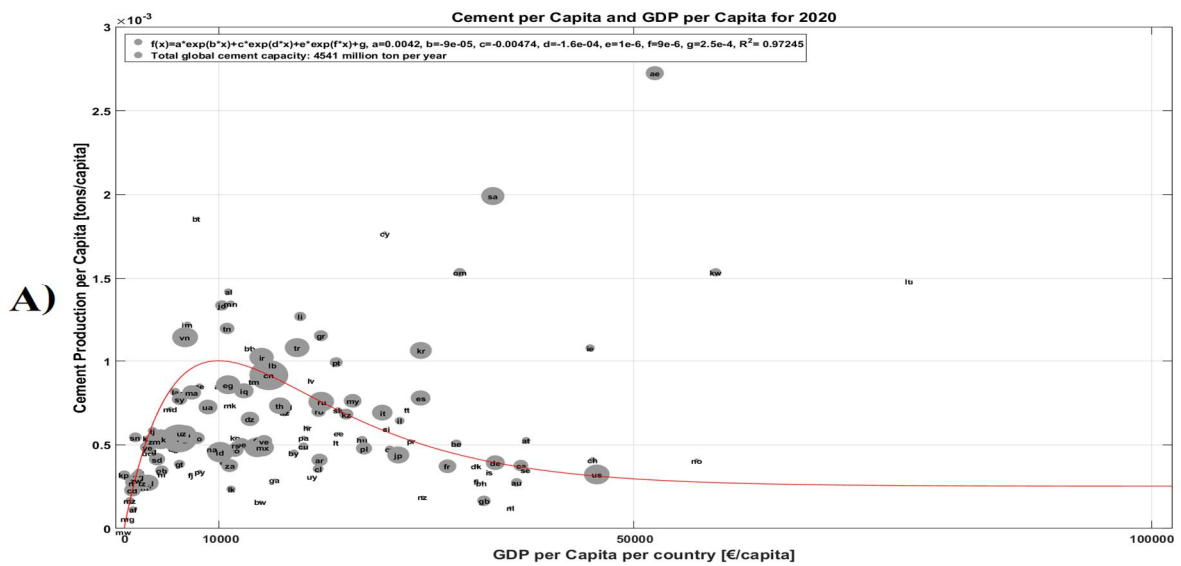
Due to the high global cement demand, a CO₂ emissions mitigation strategy should be implemented in order to achieve greater sustainability, much more than what is already planned to be implemented [25]. Several strategies are available for cement GHG emissions reduction. From relatively simple ones like using renewable electricity and waste as alternative fuel [3, 5, 39, 40], CCS [41], and even CCU for producing carbon nanotubes [42]. Usón et al. [40] provided an overview on alternative fuels usage and mentioned Norway, Germany and Austria

reaching an alternative fuel ratio in cement production of 60.0%, 62.0% and 63.1%, whereas the Netherlands achieved 83% replacement of fossil fuels with waste materials. Usón et al. also report on the relative H₂ share of syngas from various wastes, such as 42.7% (municipal solid waste), 45.5% (biomass) and 51.5% (tyres).

Cao et al. [43] further reinforced the finding of GDP and infrastructure development dependency of cement per capita demand. For this reason developing countries (India, Philippines, China, Mexico, Vietnam, etc.) experience higher per capita demand of cement than developed countries (Norway, United States, Netherlands, Denmark, Japan, etc.) as shown in Figure 5.

3.2. Future projections

Based on the GDP and infrastructure dependency premise, Figure 8 shows a projection of the global cement production capacity demand by country for 2020, 2030, 2040, 2050. The GDP projection is taken from Toktarova et al. [44]. The cement production capacity per capita and total capacities are adjusted to the growing GDP, as the circles of each country approach the steady state of the projection line.



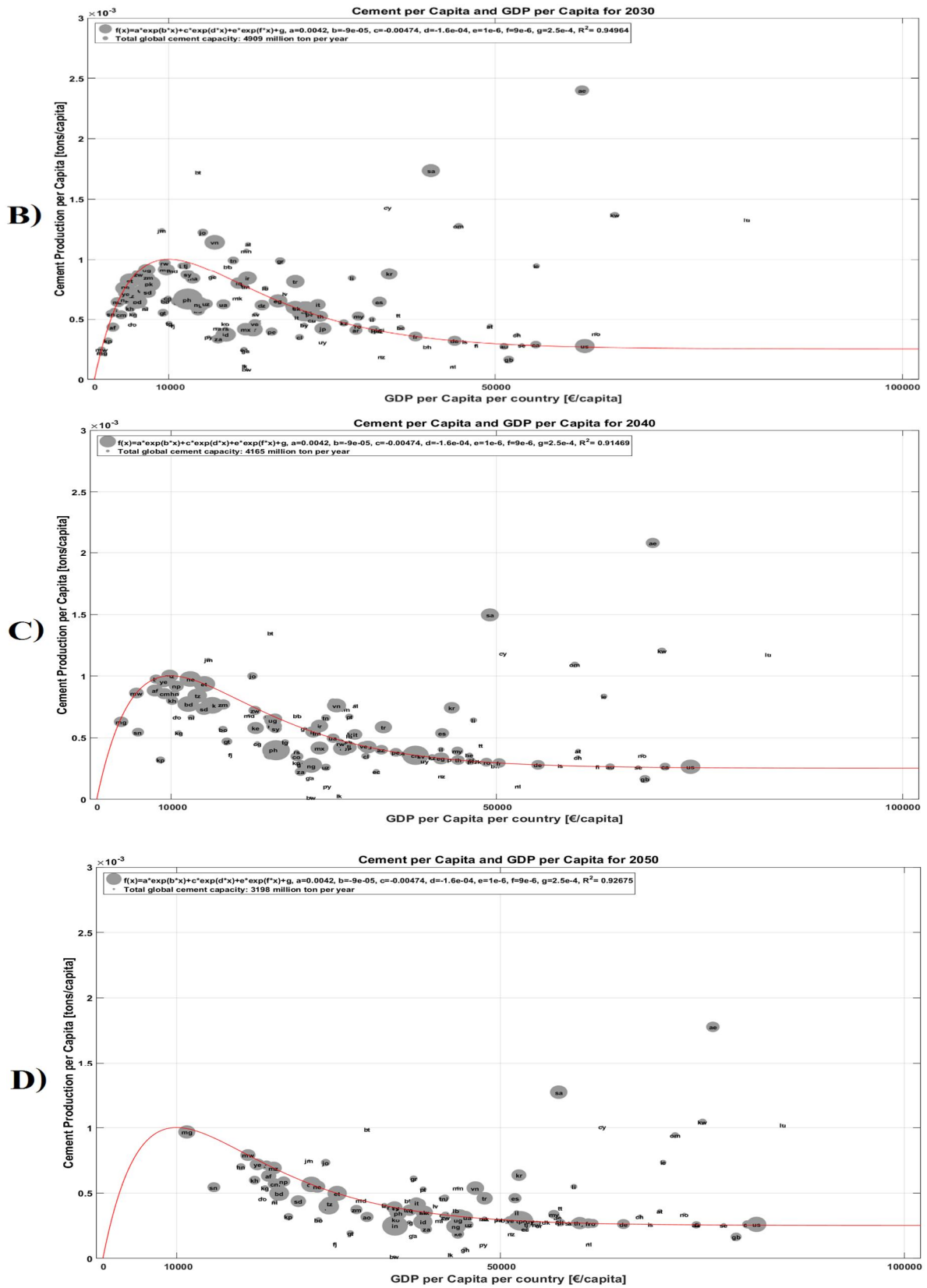


Figure 8: Distribution of cement per capita over GDP per capita globally for 2020 (A), 2030 (B), 2040 (C) and 2050 (D).

As shown in Figure 8, due to the expected development of Asian, African and Latin American countries (and despite China reducing steadily its production) the global cement production

capacity demand is expected to increase from 3885 Mt in 2014 to 4541 Mt in 2020, and further to 4909 Mt in 2030. The global production is then expected to decrease to 4165 Mt in 2040 and 3198 Mt in 2050, reaching finally below current levels of demand.

3.3. Power-to-X potential

By 2050, and according to the calculations, the potential of captured CO₂ for PtX use would be distributed globally as shown in Figure 9. Using the aforementioned methods for CO₂ utilisation, the potential for fuel production based on HHV and the additional demand of electricity and hydrogen to generate the desired fuels are displayed in Table 5. Most of the additional electricity demand is for hydrogen production through electrolysis. It can be noticed that (due to projected global cement demand) the peak potential for PtX production is reached in 2040 for all scenarios, (at a maximum of about 7355 TWh_{th} or 12723 TWh_{th} of liquid hydrocarbons and SNG respectively for BAU, 5555 TWh_{th} or 9599 TWh_{th} for CSIIt, 4209 TWh_{th} or 7288 TWh_{th} for BCSa, and 3639 TWh_{th} or 6298 TWh_{th} for BCSe).

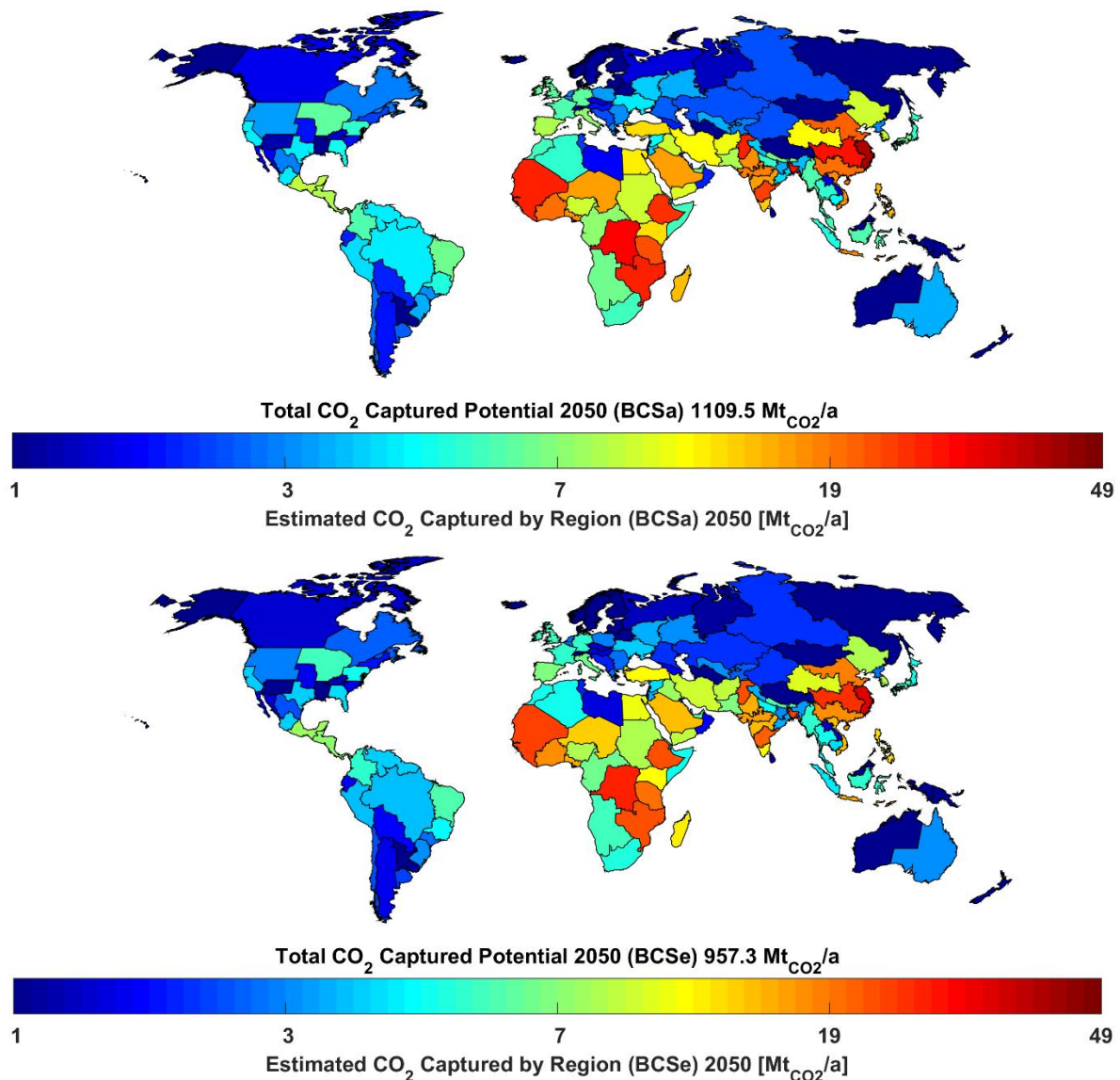


Figure 9: Estimated captured CO₂ by region by 2050 according to BCSa (top) and BCSe (bottom).

Table 5: Estimated synthetic fuel production potential based on CO₂ emissions for the different defined scenarios for a carbon capture ratio of 60% for the years before 2030, and 70% and 80% for 2040 and 2050 respectively in all cases. The input electricity is mainly used for the hydrogen production.

Input		PtL				PtG				Difference to 2015 in %
Output	year	MtCO ₂	H ₂ TWh	TWh _e	TWh _{th}	MtCO ₂	H ₂ TWh	TWh _e	TWh _{th}	
BAU	2015	1672	8524	10515	5438	1672	11929	14366	9397	0%
	2020	1961	9997	12332	6377	1961	13989	16847	11020	15%
	2030	2199	11211	13830	7152	2199	15689	18893	12358	24%
	2040	2262	11530	14223	7355	2262	16151	19451	12723	26%
	2050	1938	9881	12189	6303	1938	13827	16652	10892	14%
CSIt	2015	1263	6437	7941	4107	1263	9009	10850	7097	0%
	2020	1481	7549	9313	4816	1481	10565	12724	8323	15%
	2030	1661	8466	10444	5401	1661	11849	14269	9334	24%
	2040	1708	8707	10741	5555	1708	12186	14675	9599	26%
	2050	1464	7462	9205	4760	1464	10441	12574	8225	14%
BCSa	2015	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	Difference to 2030 in %
	2020	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	
	2030	1259	6416	7914	4093	1259	8996	10834	7087	0%
	2040	1294	6598	8140	4209	1294	9252	11142	7288	3%
	2050	1109	5654	6975	3607	1109	7929	9548	6246	-13%
BCSe	2015	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	Difference to 2030 in %
	2020	n/a	n/a	n/a	n/a	n/a	n/a	n/a	n/a	
	2030	1088	5546	6842	3538	1088	7753	9337	6107	0%
	2040	1119	5704	7037	3639	1119	7995	9628	6298	3%
	2050	959	4888	6030	3118	959	6841	8238	5389	-13%

The distribution of the synthetic fuels production potential across the global regions is presented in Table 6. Though the global synthetic fuels production potential (shown in Table 5) peaks in 2040, the tendencies for every individual region differs broadly. A steep constant decrease is projected for Northeast Asia and a slight decrease for Europe, regions which already have deployed most of the required infrastructure. SAARC (South Asian Association for Regional Cooperation) and Sub-Saharan Africa experience a well-defined ‘rise-and-fall’ tendency, peaking in 2030 and 2040 respectively. The rest of the regions go through a rather flat development over the years, with small variations in potential from decade to decade, increasing or decreasing by small amounts.

Six out of the nine regions (excluding Europe, Eurasia and Northeast Asia) are projected to have a higher CCU-PtX potential (due to cement demand) than in 2015. From these regions, only SAARC and Sub-Saharan Africa have a significant increase in potential to 2015 levels for a factor of two and eight respectively. On the contrary, Northeast Asian potential drops by around 50%, while Europe and Eurasia drop by roughly 30% and 40% respectively. The rest of the world regions experience almost insignificant increase or decrease in potential from an absolute value point of view, but not more than +/- 20% in relative values. Overall, the global potential of PtX increases by 16% by 2050 compared to 2015 values, mostly due to the assumed increase in carbon capture efficiency as the global cement production is expected to decrease.

Table 6: Estimated synthetic fuel production potential in regional distribution for all scenarios.

Region	PtL [TWh _{th}]					PtG [TWh _{th}]				
BAU	2015	2020	2030	2040	2050	2015	2020	2030	2040	2050
Europe	583	550	464	435	414	1009	951	802	751	715
Eurasia	225	231	213	165	142	390	399	368	285	245
MENA	590	636	647	635	596	1020	1100	1119	1097	1030
Sub-Saharan Africa	209	505	1336	2014	1688	362	873	2311	3482	2918
SAARC	658	1237	1845	1776	1218	1138	2139	3191	3070	2106
Northeast Asia	2122	2021	1443	1158	1049	3668	3493	2495	2002	1814
Southeast Asia	462	583	630	555	542	799	1008	1090	960	938
North America	273	261	242	289	327	472	451	418	499	566
South America	296	331	312	323	316	511	572	540	559	546
Total Global	5438	6377	7152	7355	6303	9397	11020	12358	12723	10892
	PtL [TWh _{th}]					PtG [TWh _{th}]				
CSIt	2015	2020	2030	2040	2050	2015	2020	2030	2040	2050
Europe	441	415	350	328	312	762	718	606	567	540
Eurasia	170	174	161	124	107	294	302	278	215	185
MENA	445	480	489	479	450	770	831	845	828	778
Sub-Saharan Africa	158	381	1009	1519	1275	273	659	1745	2627	2204
SAARC	497	934	1394	1340	920	859	1615	2410	2316	1590
Northeast Asia	1602	1526	1090	874	792	2771	2638	1884	1510	1370
Southeast Asia	349	440	476	419	410	604	762	823	724	708
North America	206	197	183	218	247	357	341	316	377	427
South America	223	250	236	244	238	386	432	408	422	412
Total Global	4107	4816	5401	5555	4760	7097	8323	9334	9599	8225
	PtL [TWh _{th}]					PtG [TWh _{th}]				
BCSa	2015	2020	2030	2040	2050	2015	2020	2030	2040	2050
Europe	n/a	n/a	266	249	237	n/a	n/a	460	430	410
Eurasia	n/a	n/a	122	94	81	n/a	n/a	211	163	141
MENA	n/a	n/a	371	364	342	n/a	n/a	642	629	591
Sub-Saharan Africa	n/a	n/a	766	1154	968	n/a	n/a	1325	1995	1673

SAARC	n/a	n/a	1058	1017	698	n/a	n/a	1830	1759	1208
Northeast Asia	n/a	n/a	827	663	602	n/a	n/a	1431	1147	1040
Southeast Asia	n/a	n/a	361	318	311	n/a	n/a	625	550	538
North America	n/a	n/a	139	165	188	n/a	n/a	240	286	324
South America	n/a	n/a	179	185	181	n/a	n/a	309	320	313
Total Global	n/a	n/a	4093	4209	3607	n/a	n/a	7087	7288	6246
	PtL [TWh _{th}]					PtG [TWh _{th}]				
BCSe	2015	2020	2030	2040	2050	2015	2020	2030	2040	2050
Europe	n/a	n/a	229	215	205	n/a	n/a	396	372	354
Eurasia	n/a	n/a	105	82	70	n/a	n/a	182	141	121
MENA	n/a	n/a	320	314	295	n/a	n/a	553	543	510
Sub-Saharan Africa	n/a	n/a	660	997	835	n/a	n/a	1142	1724	1444
SAARC	n/a	n/a	912	879	603	n/a	n/a	1577	1520	1042
Northeast Asia	n/a	n/a	713	573	519	n/a	n/a	1233	991	897
Southeast Asia	n/a	n/a	312	275	268	n/a	n/a	539	475	464
North America	n/a	n/a	119	143	162	n/a	n/a	207	247	280
South America	n/a	n/a	154	160	156	n/a	n/a	267	277	270
Total Global	n/a	n/a	3538	3639	3118	n/a	n/a	6107	6298	5389

4. Discussion

Replacing cement and concrete by alternative substances or materials, like magnesium based concretes [16], has not yet been commercially developed or thoroughly tested and cannot realistically be considered to eliminate the emissions from cement production. Therefore, because half of the cement related GHG emissions originate directly from the limestone, CCU appears to be so far the only viable option to at least mitigate the GHG emissions in cement production. It would only reduce final GHG emissions if fossil fuels were substituted, which will be not anymore possible after the full ban of fossil fuels, which is a clear consequence of the Paris Agreement. Zhou et al. [41] pointed out, though in concept carbon capture is applicable to cement processing facilities, it is not yet widely used or even commercially available. Further development and demonstration on this topic is still required, but should be eventually accomplished. Also, for the BCSe and BCSe scenarios electricity from a fully renewable energy based system is assumed. While this is in principle possible [10, 11, 15] the evolution of the global energy system is still not certain.

A new strategy for cement CCU has been presented, and the regional and global potential from PtX has been shown. Different demands for the captured CO₂ may balance the supply: rather passive applications such as enrichment of greenhouse horticulture [45] or concrete curation [46], to rather complex techniques like carbon nanotubes synthesis [41], liquid and gaseous hydrocarbon generation [11, 47], plastics [48] and a wide range of usable chemicals [17, 49, 30] and other applications such as mineral carbonation [35], etc. Furthermore, it could also be expected that new technologies and uses for captured CO₂ will be developed over time. Nevertheless, the main demand sectors by volume are most likely to be synthetic fuels (liquid and gaseous) and chemicals.

In addition, the actual impact of synthetic fuels on the overall emissions of the cement industry could be discussed. Are CO₂ emissions avoided or just postponed? Converting the captured CO₂ into an energy carrier for later use eventually releases the captured carbon. However, synthetic fuels from captured carbon not only replace directly the emissions from the utilisation of fossil derived fuels that would have been used otherwise, but also completely avoid the emissions associated with the extraction and refining of fossil fuels. In literature, there are discussed three main techniques for carbon capture from cement and respective mitigation, which are post-combustion scrubbing CCS, oxy-combustion CCS and calcium looping plus oxy-combustion [22, 50, 51]. The carbon capture efficiencies assumed in the presented work are within the boundaries of 60% efficiency set by [52] and the 70% assumption made by [53], and the maximum efficiency of 94% reported by [22]. Efficiency for carbon capture from cement can be rather controversial, since as pointed out by [54], carbon capture has so far been applied only in one case (and reference is not available for the case). Efficiencies up to 94% have been estimated [55], but in research with such high reported efficiencies the assumptions are often questionable or important factors, such as fuel derived emissions, additional materials derived emissions, etc. are left out. The carbon capture efficiencies are assumed as 60%/ 70%/ 80% for before 2030/ 2040/ 2050 respectively, as carbon capture becomes an integral part of the cement making process, the whole process could be better adapted to CCU.

Therefore, still after carbon capture, 40%, 30% and 20% of the raw material derived emissions would be directly released before 2030, 2040 and 2050 respectively. However, up to 43% of the raw material derived emissions (or around 21% of the current total emissions over an 83 years period [16, 56]) is eventually absorbed by the concrete over its operational lifetime. The remaining 60% of the limestone-derived CO₂, after being captured and utilised in hydrocarbons production (potentially displacing fossil-originated CO₂ emissions), would be eventually emitted to the atmosphere, but still the total emissions from the cement process would be reduced by 70% compared to the BAU scenario. Over time, as carbon capture becomes an integral part of the cement production process, it is expected that adaptations can be made to significantly increase the efficiency of carbon capture, or even new better technologies could be developed.

Carbon capture (CC) from cement mills is in competition with CO₂ direct air capture (DAC) [57, 58]. A cheaper source of CO₂ would result in lower synthetic fuels production costs. The projected final costs for both technologies shows a great variance in literature. However, due to higher concentration of CO₂ in flue gases, the carbon capture process at cement mills is most likely lower in cost than the major alternative CO₂ direct air capture, which in turn can reduce the synthetic fuel production cost.

Carbon capture from cement mills, depending on the technology, increases the energy consumption by 0.3-1.4 MWh per ton of captured CO₂, and a cost of 13-124 € per ton of

captured CO₂ [51]. Oxy-combustion with calcium looping is considered as one of the cheapest options. In a cement mill with carbon capture coupled to PtX, oxy-combustion technologies would benefit from the excess oxygen produced in the electrolyser unit required for the PtX processes. The oxy-fuel combustion needs less fuel, as the heat loss related to nitrogen heating would be avoided. Avoiding nitrogen would decrease the volume of flue gases, which would also lower cost of the plant due to smaller flue gas facilities. In addition, CC cost would also decrease because of a smaller volume of flue gases with a higher density of CO₂.

On the other hand, the reported costs for DAC are relatively higher, in the range of 150 to 300 €/per ton [59-64] (the amounts reported originally in USD are converted to € at a 1 € to 1.33 USD conversion rate, for the purpose of this work). Climeworks, as a forerunner in this field, expects to reduce the costs to 75 €/per ton for large-scale DAC farms [63]. Moreover, some literature suggests costs below that, down to 45 €/per ton [65, 66] or even lower to 40 - 60 €/t_{CO2} by 2050 [58], which could be confirmed for the Maghreb region in the first hourly modelling of CO₂ capture [11]. The current consensus on the price of cement is 26 €/per ton of cement for dry kiln process with precalciner [50]. In addition, the impact of energy cost would be minimised for a DAC unit with low temperature energy demand coupled by PtX plants, as it could receive about 87% of its energy demand from excess heat of synthesis units. Thus, higher electricity prices would not have a major impact on DAC.

Although cement CC could be lower in cost than CO₂ DAC, other factors for cheaper synthetic fuel production should be also taken into account. Access to relatively low-cost electricity with high full load hours (FLh) at the location of cement mills is crucial for low-cost hydrogen generation, as the other feedstock for fuel production happens to have a bigger impact on the final costs of synthetic fuels. As an example, for an electricity cost of 24 €/MWh and 6480 FLh and a CO₂ cost of 20 or 42 €/ton in 2030, SNG could be generated for a final cost of 53 or 57 €/MWh, respectively. However, such a good levelised cost of electricity (LCOE) and FLh may not be achievable in most parts of the world. An LCOE of 40 €/MWh with the same FLh, may have a relatively small impact on CO₂ capture cost, but would increase the SNG generation cost to 78 and 82 €/MWh, respectively. Meanwhile DAC units could be located at the best electricity generation sites in the world. With the electricity generation equal to the first case and a CO₂ cost of 100 €/t_{CO2}, SNG could be produced for a cost of 67 €/MWh, which is relatively cheaper. In addition, it needs to be further investigated whether it is appropriate to allocate the PtX plants close to the cement mills, since logistical infrastructure is needed to transport the synthetic fuels to the consumption sites. Some of the cement CCU potential may be lost due to such locational mismatches.

5. Conclusions

Carbon capture and utilisation represents an important potential approach via synthetic fuel generation from cement manufacturing process. Depending on scenarios, the fossil fuel consumption can be fully eliminated by the usage of waste and hydrogen, or a fully electric cement process. Emissions of the limestone cannot be fully compensated. Reaching a maximum potential peak in 2040, the production potential of synthetic hydrocarbon fuels from carbon captured in cement plants and electricity generated by renewables is between 3639 TWh_{th} and 7355 TWh_{th} of liquid hydrocarbons, or 6298 TWh_{th} and 12,723 TWh_{th} of SNG with the peak in 2040, globally. A considerable additional energy demand is appended in order to produce the mentioned amounts of synthetic fuels, 6030 TWh_{el} to 12,189 TWh_{el} for liquids and 8238 TWh_{el} to 16,652 TWh_{el} for SNG, respectively in 2050. However, in a future energy system dominated by variable RE sources [10, 15], the costs of electricity would be

significantly reduced. Production of synthetic fuels from captured CO₂ can be done in accordance to the variable renewable resource availability, and further complement the energy system by functioning as a “virtual” chemical energy storage, in particular due to the synthetic fuel trading potential, as already discussed for the case of the Maghreb region [11] and in East Asia [67].

According to BP Energy Outlook 2017 [68], the global oil and gas demand in 2015 were about 52,500 TWh_{th} and 38,600 TWh_{th}, respectively. These would increase to 60,300 TWh_{th} and 53,200 TWh_{th} in 2035, respectively, according to the same source. In BP’s best case scenario, 2035 could be the peak year of oil demand, with an almost even demand from 2030 to 2040. The highest synfuel generation potential from cement mill’s CO₂ emissions in 2040 is about 15% of oil demand or 28% of gas demand in 2035. Nevertheless, it is expected that in a world with high shares of synthetic fuels, the light to medium transportation sector would be electrified and the oil demand for power generation is already substituted by renewable electricity. The electrification of marine, aviation and some parts of the industry would be still complicated or impossible, therefore a substantial hydrocarbon demand will remain even in a net zero GHG emissions scenario matching the Paris Agreement. However, only the non-energetic demand for oil and gas in 2035 is expected to be around 10,600 TWh and 3600 TWh, respectively. This non-energetic oil demand solely exceeds the synfuel generation potential from cement CO₂ emissions. Moreover, since the use of CCU for PtX does not entirely eliminate the CO₂ emissions from the cement production, alternative uses for the CO₂, or even alternatives to traditional cement and concrete, should be considered. In the discussion section, an array of options for CO₂ utilisation is presented, as well as some of the alternatives to limestone for cement production. Moreover, the constant ongoing research on construction materials may provide more sustainable alternatives in the future.

The majority of PtX production potential (67%) at the 2040 projected peak is concentrated in the SAARC region, Sub-Saharan Africa (ramping up) and Northeast Asia (despite the continuous decrease). Northeast Asia, dominated by China, experiences a reduction in synthetic fuel production potential from almost 39% of the global potential in 2015, down to less than 17% in 2050. North and South America show a rather stable potential throughout the projected years, while Eurasia, Europe and Northeast Asia experience a significant reduction in their synthetic fuel production potentials by 2050. The largest overall growth in synthetic fuel production potential by 2050 compared to 2015 can be expected for Sub-Saharan Africa, in the order of 800%.

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