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Production and characterization of coffee-pine wood residue briquettes as an alternative fuel for local firing systems in Brazil

Mendoza Martinez Clara Lisseth, Sermyagina Ekaterina, de Cassia Oliveira Carneiro Angélica, Vakkilainen Esa, Cardoso Marcelo

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5 **1 PRODUCTION AND CHARACTERIZATION OF COFFEE-PINE WOOD RESIDUE**
6 **2 BRIQUETTES AS AN ALTERNATIVE FUEL FOR LOCAL FIRING SYSTEMS IN**
7
8 **3 BRAZIL**
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10 *Clara Lisseth Mendoza Martinez^{abc*}, Ekaterina Sermyagina^b, Angélica de Cassia Oliveira*
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13 *Carneiro^c, Esa Vakkilainen^b, Marcelo Cardoso^a*
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17 ^aFederal University of Minas Gerais (UFMG), Belo Horizonte, MG Brazil, 31270-901

18 ^bLappeenranta University of Technology, Skinnarilankatu 34, FI-53850 Lappeenranta, Finland

19 ^cFederal University of Viçosa (UFV), Viçosa, MG, Brazil, 36.570-000
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25
26 **10 ABSTRACT** - In this work, the production viability, physical, chemical and mechanical
27 properties of briquettes produced from mixtures of coffee shrub residues and pinewood, were
28 evaluated. The densification was carried out under constant operating conditions (temperature of
29 120 °C, pressure of 8.27 MPa) in a piston-press type laboratory-scale briquetting machine.
30
31 120 °C, pressure of 8.27 MPa) in a piston-press type laboratory-scale briquetting machine.
32
33 14 Coffee shrub residues were mixed with pinewood in ratios of 25%, 50% and 75%. In addition,
34 reference briquettes of pure pinewood and of each type of coffee shrub residue were produced.
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36 16 To characterize the raw material, ash content, volatile matter, fixed carbon together with the
37 calorific value of produced samples, were measured. To characterize the suitability of the
38
39 17 briquettes produced: apparent density, energy density, tensile strength, and equilibrium moisture
40
41 18 content were determined. The highest values of energy density (19133 – 19899 MJ·m⁻³), tensile
42
43 19 strength (415 – 569 kgf), apparent density (1107-1163 kg·m⁻³) and favorable values of
44
45 20 equilibrium moisture content (9 – 11 wt %) were obtained from a mixing ratio of 75% of
46
47 21 pinewood. The novel contribution of this research was to develop briquettes with appropriate
48
49 22 physical and mechanical parameters from new raw materials that could serve as sustainable fuel
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51 23 sources for local firing systems.
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54 **25 Keywords:** Densification; coffee residues; pinewood; briquette; physical properties
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60 *Corresponding Author at: School of Chemical Engineering, Federal University of Minas Gerais, room 5210, block 2, 6627 Antonio Carlos
61 Road, 31270901, Belo Horizonte, Minas Gerais, Brazil.
62 E-mail address: clara.mendoza.martinez@gmail.com
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1. INTRODUCTION

In brazil, utilization of biomass from agriculture, agroindustry and forestry are advantageous as their availability is not hindered by a requirement for arable land for food and feed production [1]. It is estimated that more than 200 million tons from agroindustry residues are not utilized energetically, mainly due to their poor energy characteristics: e.g. low density, low heating value and high moisture content [2]. In order for biomass to be considered for implementation as a viable fuel, it must be transformed into a readily useable and high energy resource.

Technologies that can transform firewood, agroforestry and industrial residues into a final product with high potential properties are attractive for the Brazilian energy matrix. One alternative to conventional energy sources is the utilization of pressed residues in the form of briquettes or pellets. Thus, the proper densification contributes to high volumetric concentration of energy, improving the handling and reducing the volume and resulting storage and transport costs [3]

1.1 Biomass briquetting in brazil

Briquettes have long been used by residences, industries and commercial establishments, substituting for considerable quantities of firewood that would otherwise be extracted from the forest, thereby reducing negative environmental impacts. Briquettes in Brazil are used as substitutes for firewood in bakeries, food establishments, pizza restaurants, as well as factories with fuelwood-burning furnaces, like red brick factories [4], [5]. Briquetting activities in Brazil are limited to those few regions with high wood residues concentrations, such as the states of Sao Paulo, Santa Catarina and Mato Grosso [5]. Nevertheless, the quest for sustainability and the so-called green economy has contributed to expanding consumption, and consequently, the production of briquettes. This expansion primarily depends on three factors: residue availability, adequate technologies and a growing market for briquettes[5].

Briquetting presents an efficient densification process that produces a uniform fuel, increases the energy density and reduces the transport and handling costs of the biomass residues [6], [7]. The briquettes are generally produced in a piston (mechanical or hydraulic) press by applying load on a die with biomass particles. Additional binder and heat treatments can be applied

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4 55 depending on the properties of the feedstock [5]. To evaluate the final product, resistance to
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6 56 compression, energy density, compaction rate and equilibrium moisture, among others
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8 57 properties, should be measured [8].
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10 58 Several studies have evaluated the possibility of utilizing different agricultural wastes and by-
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12 59 products for briquetting. A number of authors have investigated rice residue potential: analyzing
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14 60 the briquettes from rice straw and rice bran [10]–[12]; briquetting of rice and coffee husks for
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16 61 domestic cooking applications [13]; production of activated carbon briquettes from rice husks
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18 62 and eucalyptus wood [14]. Very positive results were obtained from blends of rice husks with
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20 63 corn cobs [15], [16] and other residues of corn [17], [18]. This rational use of biomass tends to
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22 64 promote the development of less economically favored regions, through the creation of jobs and
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24 65 reduction of external energy dependence, based on their local availability. The advantage of
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26 66 briquettes being manufactured from industrial and agroforestry residues is that their resulting
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28 67 price is lower compared to a large variety of fuels: e.g. charcoal [3], [9].
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30 68 **1.2 Coffee residual biomass potential**

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32 69 The coffee production chain generates a large quantity of residues from both the berries
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34 70 (beans) themselves and the shrub. It is estimated that over ten million tons of residues yearly
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36 71 (solid and liquid) are produced [19]. In addition, there are residues from cultivation (pruning),
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38 72 which are difficult to estimate due to the differences in agronomic management practices. Brazil
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40 73 is the largest producer and exporter of coffee in the world. About 2.78 million tons of coffee
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42 74 beans were produced in 2016-2017. From this production , approximately 2.3 million tons of
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44 75 solid residues are generated each year [20]. Currently, these residues; coffee pulp, parchment,
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46 76 coffee wood and effluents, are not utilized efficiently and can result in severe environmental
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48 77 impacts due to inappropriate disposal [21]. The disposal of coffee wastes remains a challenge
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50 78 due to the presence of caffeine, free phenols and tannins (polyphenols), which are even toxic to
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52 79 many forms of life [22]. Currently, only a small fraction of available coffee pulp and parchment
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54 80 is utilized; as fertilizers, livestock feed, etc. The possibility of improving the properties and
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56 81 converting the waste streams into a competitive fuel in the energy market (production of solid
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58 82 fuels [briquettes, pellets and charcoal], biogas, liquid fuels) or extraction of the valuable
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60 83 chemicals from them may result in not only environmental but economic benefits as well. For
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4 84 this reason, it is necessary to develop the pretreatment technologies to improve the biomass
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6 85 feedstock characteristics and make it more suitable for energy or chemical applications.
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9 86 As for coffee by-products themselves, there is still very little information about the energy
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11 87 potential and specific characteristics of the treatments for the residues from the coffee production
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13 88 chain. Only a few works present some results on the possible utilization pathways for these
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15 89 materials. One study [23] analyzed a process of anaerobic co-digestion of coffee husks and
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17 90 microalgal biomass after thermal hydrolysis pretreatment. In another work, high temperature air-
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19 91 steam gasification of coffee husks was studied experimentally [24]. Another group of researchers
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21 92 provided the results of their two-dimensional CFD simulation of the coffee husks' gasification in
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23 93 a fluidized bed reactor [25]. In addition to the residues typically associated with coffee
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25 94 production, the coffee chain provides another potentially abundant energy source, coffee wood
26
27 95 [26]. Ethanol fermentation and gasification of coffee wood were evaluated by [27]. Additionally,
28
29 96 it was proven that gasification represents a promising way to convert coffee wood into energy
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31 97 with high energy yields and resultingly low environmental impacts.

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33 98 According to [26], the energy potential of coffee residues - coffee husk and coffee wood - in
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35 99 Brazil is highly significant with annual available energy of 11.3 PJ and 49.5 PJ, correspondingly.
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37 100 More information is needed to choose the most optimum treatment technology for these residues.
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39 101 Use of coffee residues along with traditional biomasses already utilized in the production of
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41 102 briquettes, such as pinewood, may considerably improve the potential of coffee residue
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43 103 utilization. Pine cultivation areas occupy a rather significant landmass in Brazil with $1.58 \cdot 10^6$ ha
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45 104 planted in 2015, so the availability of feedstock would not be a limiting factor [28]. Additionally,
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47 105 pinewood is rich in natural resins that increase its calorific value [29]. It also has a high lignin
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49 106 and silica content in its composition. Briquettes production would not require any additional
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51 107 binders since lignin acts as a natural binding material during the pressing process. The present
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53 108 work analyses the viability of a briquetting process for the mixture of residues from the coffee
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55 109 production chain and pinewood to produce a solid fuel of regular shape and high energy density
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57 110 and resistance, for use in local firing systems.

58 59 60 61 62 63 64 65 66 67 68 69 70 71 72 73 74 75 76 77 78 79 80 81 82 83 84 85 86 87 88 89 90 91 92 93 94 95 96 97 98 99 100 101 102 103 104 105 106 107 108 109 110 111 **2. MATERIALS AND METHODS**

2.1 Materials

Three biomass materials were studied: coffee wood, the coffee berry parchment layer (this covers the coffee beans and represents about 12 wt % of the berry on a dry basis) and pinewood. The coffee (*Coffea Arabica* L.) residues were provided by a rural farm in the municipality of Paula Cândido, Minas Gerais state, Brazil (20°49'50.0" S 42°55'03.3" W). The plant cultivation was established in 1986, and due to low productivity, stumping of new plant formation was required. The wood collected was 11 years old (from subsequent to the last stumping period). The coffee wood samples were separated into (I) stems, (II) primary branches and (III) secondary branches according to their diameter, 10 ± 2 cm, 2 ± 1 cm and 1 ± 0.5 cm, respectively. The three components were considered separately mainly due to coffee shrub aerial morphology, which is related to two types of burgeon: ortho-tropics (coffee beans grown on the stem) and plagiotropic (coffee beans grown on the branches). In addition, previous analysis had revealed chemical differences between coffee stem, primary and secondary branches [30]. The pinewood residues were collected at the commercial cultivation sites of the experimental units of the Federal University of Viçosa, Minas Gerais State, Brazil (20°45'14" S 42°52'55"). The wood collected was 7 years old (from subsequent to the last stumping period).

The research from the experiments presented in this work was composed of two stages:

- i) Classification, physical and chemical characterization of biomasses;
- ii) Production of briquettes and their physical, mechanical and chemical characterization.

2.2 Classification and characterization of biomass feedstock

All biomasses were initially ground in a Weg® electric hammer mill at a fixed speed of $368.6 \text{ rad}\cdot\text{sec}^{-1}$, which was coupled with a 2 mm opening sieve. For the samples intended for proximate analysis, the particle size was further reduced using a Thomas model 4 Wiley® knife mill with a fixed speed of $83.7 \text{ rad}\cdot\text{sec}^{-1}$ at 60 Hz. The biomasses were finally classified into superposed sieves with openings of 40 mesh (0.47 mm) and 60 mesh (0.31 mm) according to German Institute for Standardization (DIN) EN 14780, 2017 routine procedure [31].

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4 139 The moisture content (MC) was determined according to DIN EN 14774-1, 2010 standard
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6 140 procedure [32], by keeping the sample in an oven at 105 ± 2 °C until the constant mass was
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8 141 obtained. The ash content (AC) was determined according to DIN EN 14775, 2012 standard
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10 142 [33], as the residue after complete combustion by the gradual heating of the sample in the muffle
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12 143 oven with the maximum temperature of 550 °C. The volatile matter (VM) was measured as mass
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14 144 loss after devolatilization of the samples in the oven at 900 °C according to DIN EN 15148, 2010
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16 145 standard [34]. The fixed carbon (FC) was calculated as the difference between 100 and the sum
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18 146 of all measured components.

19
20 147 The bulk density was measured with the standard procedure presented in DIN EN 15103,
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22 148 2010 [35]. The higher heating value (HHV) was obtained using an adiabatic calorimetric pump
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24 149 IKA300 according to DIN EN 14918, 2014 procedure[36].

25 26 150 **2.3 Production and characterization of Briquettes**

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28 151 The recommended moisture range of the feedstock materials before the briquetting process
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30 152 varies from 8 wt % to 15 wt % on a wet basis (wb). In this work, the biomass samples were dried
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32 153 in an oven at 25°C, until reaching 8 ± 0.5 wt % (wb) of moisture content. The initial moisture of
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34 154 the samples was 20 wt %, 17 ± 5 wt % and 12 wt % (wb) for pinewood, shrub coffee woody
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36 155 parts and parchment, respectively. The briquettes were produced in a piston-press type of the
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38 156 laboratory-scale briquetting machine from Lippel®, model LB 32. The briquetting conditions
39
40 157 were defined experimentally from preliminary tests carried out in the laboratory. The materials
41
42 158 were compressed for 4 min at a temperature of 120 °C and pressure of 8.27 MPa with a
43
44 159 subsequent cooling for 8 min. Pinewood was mixed in ratios of 25%, 50% and 75% with stem,
45
46 160 primary branch, secondary branch and a mixture of all woody parts of coffee shrub, and coffee
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48 161 berry parchment. The presence of stems, and primary & secondary branches were proportional in
49
50 162 the mixture of all woody parts. At the end of the homogenization of the biomasses, 20 g of
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52 163 mixture was weighed and placed in a steel capsule (10 cm long and 3 cm in diameter) in the
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54 164 briquetting machine. 10 briquettes per treatment were manufactured.

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56 165 After cooling, the briquettes were kept in an air-conditioned chamber at a temperature of $23 \pm$
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58 166 1 °C and a relative humidity of $60 \pm 10\%$ until equilibrium moisture content was reached. Visual
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60 167 analysis was taken both before and after conditioning in the climatic chamber to verify the visual
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62 168 appearance of the briquettes.

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4 169 The equilibrium moisture content (EMC) was determined by mass difference. Equilibrium
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6 170 was considered as having been reached when the sample mass difference between two
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8 171 successive days was less than the balance accuracy. Apparent density was measured in triplicates
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10 172 by the mercury immersion method according to [37]. The relation between the apparent density
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12 173 of the briquette, and the bulk density of the ground biomass calculated compact rate. The net
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14 174 heating value (NHV), was determined using the equation (1), according to DIN EN 14918 [36]:

$$15 \quad NHV = [(HHV - 54 \cdot H) \cdot (1 - EMC)] - (600 \cdot EMC) \quad (1)$$

16 175
17
18 176 Where,

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21 177 HHV= High heating value ($\text{MJ} \cdot \text{kg}^{-1}$); H= Hydrogen content (wt %); EMC= Equilibrium
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23 178 moisture content (wt %)

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25 179 The energy density was obtained by the multiplication of the apparent density and the NHV.

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27 180 The tensile strength by diametrical compression for briquettes was measured in triplicates
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29 181 according to the guidelines of NBR 7222 standard with adaptations presented in [38]. The tests
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31 182 were carried out in a universal test machine, Contenco brand, UMC-300 model. The result of
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33 183 maximum load was obtained by the Pavitest software 2.7.0.7.

34 35 184 **2.4 Experimental design**

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38 185 The tests were carried out for the briquettes' composition in a completely randomized
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40 186 factorial design (5x5), considering five mixing ratios of residues (0%, 25%, 50%, 75% and
41
42 187 100%), five mixing biomasses (stem, primary branch, secondary branch, mixture of wood parts
43
44 188 and parchment) and ten replicates, yielding a total of 250 sampling units.

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46 189 The influence of the pine share in the blend with coffee residues was evaluated and subjected
47
48 190 to analysis of variance (ANOVA). The combinations with the significant differences were
49
50 191 compared with Tukey's test at a 5% probability level. Statistical analyzes were performed with
51
52 192 the help of the Statistica 8.0 program [39]

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54 193 For the results on equilibrium moisture content (wt%), maximum load (kgf), apparent density
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56 194 ($\text{kg} \cdot \text{m}^{-3}$) and energy density ($\text{MJ} \cdot \text{m}^{-3}$) properties, models were defined with the aid of R program
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58 195 for explaining the data distribution. The comparison between the treatments was done by the
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60 196 identity model test [40], according to the equation (2)

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$$Property = \beta_0 \cdot Pinewood^2 \pm \beta_1 \cdot Pinewood \pm \beta_2 \quad (2)$$

Where,

Pinewood = Pinewood ratio in the mixture (0, 25, 50, 75, 100 %)

$\beta_0, \beta_1, \beta_2$ = Regression coefficients

3. RESULTS AND DISCUSSION

3.1 Characterization of the feedstock

The biomass particle size distribution is one of the most important initial characteristics of the raw material with respect to any densification process. Table 1 shows the particles size distribution of the biomasses used for the briquettes production in this study.

Table 1. Particle size distribution of the lignocellulosic residues used in the production of briquettes.

The particle size distribution of the coffee wood residues was relatively similar. The samples had a high percentage (45.1 - 51.2%) of particles with diameters of less than 0.31 mm, which passed through both 40 and 60 mesh sieves. Between 16.6% and 22.2% of particles were retained in the 60 mesh sieve (corresponding diameter range between 0.31 mm and 0.47 mm). The bigger particles with diameter between 0.47 mm and 2 mm had a share from 26.6 to 38.3%. The coffee parchment had the lowest presence of fines among the studied materials (21.9%) and the highest share of particles with diameters between 0.47 mm and 2 mm (42.8%). Most probably, the rounded shape of the parchment particles caused the higher resistance to the trituration process and resulted in higher share of larger fractions. Such behavior may be responsible for a decrease in the material homogeneity, strength, durability and resistance of resulting briquettes [41][42]. The pine sawdust contained the highest presence of fine particles (60.3%). According to [43] and [44], the quality and volumetric density of briquettes is inversely proportional to the particle size because smaller particles in the feedstock correspond to a larger surface area for bonding during densification. The increased compacting pressure result in the biomass particles being closely packed due to a reduction of void ratio and plastic deformation of the sawdust particles, therefore resulting in higher density of the briquettes [45]. However, very

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224 small particles can lead to jamming of the briquetting machine and affect the production capacity
225 [46].

226 3.1.1. Chemical characterization

227 As the objective of this study was the production of solid biofuels, it is desirable for the
228 feedstock materials and consequently the final products to have low ash content, high energy as
229 well as fixed carbon content and low volatile matter. The main combustion properties of the
230 studied lignocellulosic residues are presented in Table 2.

231 **Table 2.** Chemical characterization of the lignocellulosic residues.

232 The feedstock moisture plays an important role in the densification process, considering that
233 water acts as both a binder and a lubricant. Material that is too dry makes the bonding between
234 the particles difficult due to the elevated frictional forces in the compression channel. Excess
235 moisture can cause explosions inside the briquette due to the formation of steam. [47] observed
236 that the moisture in the biomass increases during densification through the van der Waals forces
237 by increasing the contact area between the particles. They also concluded that low moisture
238 content (5 – 10 wt%) results in more stable, resistant and denser briquettes compared to higher
239 moisture biomasses (15 wt%). Several studies recommended that the feedstock for the
240 briquettes' production should contain a moisture content between 8 – 15 wt % (wb) [48]. [49],
241 [50] and [51] suggested low feed moisture content in the range of 8 – 12 wt % (wb) to produce
242 strong briquettes that are free of cracks. Levels above or below this would lead to densified
243 material of lower quality. [52] studied the compaction of platanus tree chips at different initial
244 moistures (5.7 - 23.9 wt%) and found that for the briquetting production it is better to use lower
245 moisture content material (up to about 12 wt%) because at higher moisture levels a sharp
246 decrease in rupture force and density occurs. The moisture content of the studied biomasses was
247 in a relatively narrow range from 8.7 wt % to 12.23 wt %, characteristic of the particulate
248 material that influenced in the absence of surface cracks and significant axial expansions in the
249 briquettes.

250 Volatile matter is the portion of the fuel that is released in form of gases when the material is
251 heated. The more volatile a fuel is, the faster it burns, and the more reactive and more easily it is
252 ignited [53]. In many domestic uses, a slow rate of burning is preferred. The typical volatile
253 matter range for general biomass is 65 – 85 wt % and 76 – 86 wt % for woody biomass [54]. In

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4 254 the current work, the woody residues had a higher share of the volatile matter than the
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6 255 parchment. Pine sawdust followed by the primary branches had the highest VM values of 82.5
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8 256 wt % and 80.7 wt %, respectively. Many other materials used in the production of briquettes,
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10 257 such as rice husk (65.5 wt %), sugarcane bagasse (73.8 wt %) [55], shea meal (66.3 wt %) [56],
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12 258 paper sludge (48.7 wt %) and coal (33.1 wt %) [57], reveal values of volatile matter lower than
13
14 259 the values found for the raw material used in this study, and due to this, the coffee residues and
15
16 260 pine wood are attractive for burning processes.

17
18 261 The fixed carbon content is inversely proportional to the volatile matter. The FC for
19
20 262 parchment was 20.1 wt % and for wood residues 14.6 wt % - 19.4 wt%. According to [58], high
21
22 263 FC indicates that the materials tend to burn more slowly, requiring longer residence time
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24 264 compared to fuels with a low FC. This suggests that briquettes containing parchment in their
25
26 265 composition may demonstrate a slower burning rate when compared to briquettes manufactured
27
28 266 with coffee wood residues.

29
30 267 The ash content implies the presence of inorganic components, mostly in the form of oxides
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32 268 [59]. Due to this, the results indicated the highest inorganic composition of the parchment (5.9 wt
33
34 269 % db) followed by the secondary coffee wood branches (4.1 wt % db). Other studied materials
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36 270 had a relatively low ash content with the minimum value being for pinewood (0.8 w t%).
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38 271 According to [60], the ash content in the feedstock does not influence the densification process
39
40 272 itself. However, an ash content greater than 10 wt % will cause wear on the equipment matrix.

41 273 The elevated heating values were relatively high for all biomasses: from 18.9 MJ·kg⁻¹ for
42
43 274 parchment to 20.7 MJ·kg⁻¹ for pinewood. In comparison with other feedstocks generally used in
44
45 275 the briquettes' manufacturing, such as rice husk (16.4 MJ·kg⁻¹) [61], wheat straw (16.4 MJ·kg⁻¹),
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47 276 timothy grass (16.3 MJ·kg⁻¹) [62], sugarcane bagasse (17.3 MJ·kg⁻¹) [55] and eucalyptus wood
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49 277 (19.0 MJ·kg⁻¹) [63], the studied samples present rather attractive materials for briquetting.
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51 278 Higher energy content increases the efficiency of the subsequent utilization of the briquettes and
52
53 279 reduces the process costs.

54 55 280 **3.1.2. Bulk density**

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57 281 Bulk density is an essential factor influencing the economic viability of biomass materials
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59 282 utilization, since it affects the transport costs and the energy density of biomass. For this reason,
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4 283 the lignocellulosic residues with higher bulk density values are more desirable for the production
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6 284 of briquettes. The average values of the bulk density of the investigated biomasses are presented
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8 285 in Fig. 1.
9

10 286 **Figure 1.** Bulk density of studied biomasses (raw material).
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15 288 The 0% proportion of pine feedstock had notably higher bulk densities than the other
16
17 289 mixtures. The 100% parchment feedstock showed the highest bulk density ($341.5 \text{ kg}\cdot\text{m}^{-3}$) due to
18
19 290 high basic density of the material and flat-shaped particles. The addition of pinewood sawdust
20
21 291 significantly decreases the density levels of all studied materials. The lowest density was
22
23 292 obtained in the case of the mixtures with 75% of pine: $45 \text{ kg}\cdot\text{m}^{-3}$ on average. The bulk density of
24
25 293 the studied biomasses (raw material) used in the production of briquettes is analogous to
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27 294 unprocessed wood residues ($250 \text{ kg}\cdot\text{m}^{-3}$) [64], ground switchgrass ($181.6 \text{ kg}\cdot\text{m}^{-3}$) [41], wheat
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29 295 straw ($97.4 - 121.3 \text{ kg}\cdot\text{m}^{-3}$), corn stover ($131.4 - 157.7 \text{ kg}\cdot\text{m}^{-3}$) and barley straw ($81 - 112.1$
30
31 296 $\text{kg}\cdot\text{m}^{-3}$) [41]. The decrease in bulk density when mixing residual biomasses from the coffee
32
33 297 production chain with pine results in such mixtures requiring compaction such as briquetting.

34 298 **3.2 Characterization of the briquettes**

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36 299 The briquettes produced from coffee residues and pinewood in ratios of 25%, 50%, 75% as
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38 300 well as the briquettes from each individual biomass sample showed satisfactory visual
39
40 301 appearance: good uniformity, absence of cracks, with smooth and shiny surfaces. The produced
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42 302 briquettes are presented in Fig. 2.
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44 303 **Figure 2.** Briquettes produced from coffee residues mixed with pinewood in different ratios.
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47 305 One way of evaluating the briquetting process is by measuring the compaction rate, which
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49 306 represents the ratio between the apparent density of the briquette (Fig. 3B) and the bulk density
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51 307 of the feedstock. Higher compaction rates indicate a higher reduction of the briquette's volume
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53 308 during the densification process, which likely results in a density gain. Table 3 shows the
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55 309 average values obtained for the compaction rate in relation to the proportion of pine.
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57 310 **Table 3.** Compaction rate of the briquettes produced with studied biomasses.
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4 311 It was observed that the pinewood briquettes have a compaction rate nearly three times
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6 312 higher than the ones produced from the residues without pine addition. This is due to the
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8 313 significant difference between the bulk densities of the materials: lower bulk density increases
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10 314 the likelihood of compressing the material. As a result, the compaction rate of the mixtures with
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12 315 75% of pinewood and 25% of coffee residues showed the highest values in volume reduction.
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14 316 The residues with higher initial density would require higher energy to produce the briquette
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16 317 since these materials present greater resistance to densification. In this sense, the addition of
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18 318 pinewood in briquettes, mostly at 50% and 75% can contribute to increasing the density without
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20 319 the need of spending additional energy to increase the pressure in the compaction stage.

21 320 **3.2.1 Physical – chemical characterization**

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24 321 The average values of equilibrium moisture content, compressive strength, apparent density
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26 322 and energy density of briquettes are illustrated in Fig. 3.

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28 323 **Figure 3.** Properties of briquettes produced with the studied biomasses: equilibrium moisture
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30 324 content (upper-left), apparent density (upper-right), energy density (lower-left), and compressive
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32 325 strength (lower-right).

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34 326 Equilibrium moisture content is a notably important parameter for evaluating the possible
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36 327 changes in physical conditions of biomass briquettes during storage and transportation. The
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38 328 briquettes with low equilibrium moisture content (5 – 12 wt%) are better suited for transportation
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40 329 not only with respect to the lower concentrations of water carried in the biomass material but
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42 330 also due to increased physical and mechanical resistances of such low-moisture briquettes [46],
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44 331 [65]. Additionally, a higher EMC level complicates the ignition of the fuel and leads to lower
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46 332 energy density values due to the inverse relationship between the EMC and the net heating value
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48 333 [46]. The equilibrium moisture content for the majority of the produced briquettes was observed
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50 334 to be in a relatively narrow range between 9 and 10.3 wt % with little effect from the pine
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52 335 addition (Fig. 3A). Consequently, these briquettes can be handled more efficiently during storage
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54 336 and transportation. As for the parchment, the increase of pine proportion decreased the briquettes
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56 337 EMC: from 11.9 wt % in the case of purely parchment briquettes to 10.3 wt % in the case of 75%
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58 338 of pine in the blend.

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60 340 The measurement of apparent density after densification is essential for the evaluation of the
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62 biomass potential: lower density raises the costs of transportation and decreases the energy
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4 341 density. The apparent density of the briquettes increases with the share of pine in the mixture for
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6 342 stem, primary branch, secondary branch and wood mix (Fig. 3b) from $996.7 \text{ kg}\cdot\text{m}^{-3}$ - $1054 \text{ kg}\cdot\text{m}^{-3}$
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8 343 3 to $1136.1 \text{ kg}\cdot\text{m}^{-3}$ which represents a nearly 10% increase in density. This is due to higher
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10 344 compaction rate of the briquettes with greater percentage of fines. In case of the briquettes with
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12 345 parchment in their composition, the addition of pine only slightly decreases the apparent density
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14 346 of the samples, likely due to the high basic density of the parchment. The values observed in this
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16 347 work are similar to briquettes produced with eucalypt sawdust ($1060 \text{ kg}\cdot\text{m}^{-3}$), corn residues
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18 348 ($1159 \text{ kg}\cdot\text{m}^{-3}$) and coffee husk ($1248 \text{ kg}\cdot\text{m}^{-3}$) [38].

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20 349 The energy density indicates the energy content per volume unit and affects the efficiency of
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22 350 subsequent use of the briquettes [66]. The energy density of all produced briquettes increased
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24 351 with the addition of pinewood to the coffee residuals due to the higher heating value of the pine
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26 352 (Fig. 3c). The energy density of briquettes with parchment in their composition presented the
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28 353 highest average values for high bulk density, with increments of up to $700 \text{ MJ}\cdot\text{m}^{-3}$ corresponding
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30 354 to every 25% addition of pinewood. However, the residue that showed the greatest variation in
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32 355 this property was that of primary branches with an increase of $3551 \text{ MJ}\cdot\text{m}^{-3}$ from the absence of
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34 356 pine to 75% of pine in the mixture; the increments were of approximately $1184 \text{ MJ}\cdot\text{m}^{-3}$ for every
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36 357 25% of pinewood addition.

37 358 The tensile strength of diametric compression and maximum force is related to the ability of
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39 359 briquettes to withstand mechanical impacts during storage and transport. The briquettes with low
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41 360 resistance tend to disintegrate more quickly, which can cause problems during their combustion.
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43 361 [42] concluded that the size of particles, chemical composition, lignin content, compaction rate
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45 362 and equilibrium moisture content influence the tensile strength of the briquettes. In this study, it
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47 363 was observed that the resistance to diametric compression and maximum force increased in
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49 364 conjunction with the increase of the pine briquette content for all studied materials (Fig. 3D).
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51 365 The highest values were found for the briquettes produced from pine alone. This result is
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53 366 probably due to the low volumetric expansion after the densification of the mixtures because of
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55 367 the presence of fines, low EMC and high lignin content of the pine.

56 368 **3.3 Identity model test for the physical-chemical properties measured in the briquettes**

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58 369 The obtained results confirm the similarity of the biomasses' behavior in the majority of the
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60 370 cases and likely explain the dependencies of the studied properties with the general equations.

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371 However, this is only possible for the maximum resistance property due to the covariance
372 analysis (Table 4), which reveals a higher p-value than the level of significance $\alpha = 0.05$,
373 contrary to EMC, energy density and apparent density properties.

374 **Table 4.** Covariance analysis for the properties measured in the briquettes.

375
376 As a result, the data were regrouped without the presence of the coffee berry parchment
377 for the energy density and apparent density properties. The analysis of covariance showed that
378 the equations present similar estimates in relation to the behavior of the briquettes with the
379 pinewood addition. Model identity tests for the equilibrium moisture property indicated that it is
380 not advisable to apply a single equation adjusted for the data set. Meanwhile, for stem – wood
381 and primary branch - secondary branch mixtures, a single adjusted equation can be used to
382 represent the data set of these biomasses.

383 Table 5 shows the parameters of the models for the measured properties as a function of
384 the proportion of pine wood (Eq. 2), according to the adjustments made by the model identity
385 test. These results have a significant importance, once the adjusted models could be used to
386 estimate the value of the physical–chemical properties of briquettes by varying the proportion of
387 pinewood in the mixture.

388
389 **Table 5.** Adjusted equation for the physical – chemical properties of briquettes.

392 4. CONCLUSION

393 In this study, it was demonstrated that the residues from the coffee production chain such as
394 stems, primary branches and secondary branches of coffee shrubs and the parchment of coffee
395 berries can be used to produce briquettes for combustion processes when mixed with pine wood,
396 creating a new source for the utilization of undervalued residual biomasses. The mechanical
397 strength obtained from coffee residues alone was quite low. However, when blended with pine
398 wood, strong and high-quality briquettes can be produced. The resulting briquettes present a
399 regular format and homogeneous constitution, characteristics that are indicative of better quality
400 and durable products after handling, transportation and storage. additionally, the high energy
401 density of the briquettes produced presents an attractive advantage for increasing the Brazilian
402 energy production matrix using densified material.

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408 REFERENCES

- 409 [1] V. Ferreira-Leitao, L. M. F. Gottschalk, M. A. Ferrara, A. L. Nepomuceno, H. B. C.
410 Molinari, and E. P. S. Bon, Biomass residues in Brazil: Availability and potential uses,
411 *Waste and Biomass Valorization*, 1 (2010) 65-76.
- 412 [2] L. A. B. Cortez, E. S. Lora, E. O. Gomez, *Biomassa para energia*, Unicamp, Brazil, 1st
413 Ed. 2008.
- 414 [3] F. Santos, J. L. Colodette, and J. H. de Queiroz, Bioenergia & Biorrefinaria Cana de
415 Açúcar & Espécies Florestais, UFV, Brazil, 1st Ed. 2013.
- 416 [4] J. O. dos Santos, R. M. de Sousa Santos, L. M. da Costa, A. C. de Medeiros, D. C. Coelho,
417 and P. B. Maracajá, Production and use of briquettes in Brazil, *Rev. Bras. Agrotecnologia*.
418 5 (1) (2015) 36–40.
- 419 [5] F. F. Felfli, J. M. Mesa P, J. D. Rocha, D. Filippetto, C. A. Luengo, and W. A. Pippo,
420 Biomass briquetting and its perspectives in Brazil, *Biomass and Bioenergy*. 35 (1) (2011)
421 236–242.
- 422 [6] J. Karlhager, The Swedish Market for Wood Briquettes: Production and Market
423 Development, Master Thesis, Swedish University of Agricultural Sciences, Sweden. 2008.
- 424 [7] M. Temmerman, F. Rabier, P. D. Jensen, H. Hartmann, and T. Böhm, Comparative study
425 of durability test methods for pellets and briquettes, *Biomass and Bioenergy*. 30 (11)
426 (2006) 964-972.
- 427 [8] A. Gendek, M. Aniszewska, J. Malat'ák, and J. Velebil, Evaluation of selected physical
428 and mechanical properties of briquettes produced from cones of three coniferous tree
429 species, *Biomass and Bioenergy*. 117 (2018) 173-179.

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58
59
60
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63
64
65

[9] C. S. Chou, S. H. Lin, and W. C. Lu, Preparation and characterization of solid biomass fuel made from rice straw and rice bran, *Fuel Process. Technol.* 90 (7–8) (2009) 980–987.

[10] A. Yank, M. Ngadi, and R. Kok, Physical properties of rice husk and bran briquettes under low pressure densification for rural applications, *Biomass and Bioenergy.* 84 (2016) 22–30.

[11] C. S. Chou, S. H. Lin, C. C. Peng, and W. C. Lu, The optimum conditions for preparing solid fuel briquette of rice straw by a piston-mold process using the Taguchi method, *Fuel Process. Technol.* 90 (7–8) 2009 1041–1046.

[12] M. Lubwama and V. A. Yiga, Characteristics of briquettes developed from rice and coffee husks for domestic cooking applications in Uganda, *Renew. Energy.* 118 (2018) 43–55.

[13] A. Amaya, N. Medero, N. Tancredi, H. Silva, and C. Deiana, Activated carbon briquettes from biomass materials, *Bioresour. Technol.* 98 (8) (2007) 1635–1641.

[14] R. I. Muazu and J. A. Stegemann, Effects of operating variables on durability of fuel briquettes from rice husks and corn cobs, *Fuel Process. Technol.* 133 (2015) 137–145.

[15] J. Oladeji, Fuel characterization of briquettes produced from corncob and rice husk residues, *Pacific J. Sci. Technol.* 11 (1) (2010) 101–106.

[16] A. A. Salema, M. T. Afzal, and L. Bennamoun, Pyrolysis of corn stalk biomass briquettes in a scaled-up microwave technology, *Bioresour. Technol.* 233 (2017) 353–362.

[17] N. Kaliyan and R. V. Morey, Natural binders and solid bridge type binding mechanisms in briquettes and pellets made from corn stover and switchgrass, *Bioresour. Technol.* 101 (3) (2010) 1082–1090.

[18] M. Brožek, A. Nováková, and M. Kolářová, Quality evaluation of briquettes made from wood waste, *Res. Agric. Eng.* 58 (1) (2012) 30-35.

[19] M. C. Echeverria and M. Nuti, Valorisation of the Residues of Coffee Agro-industry: Perspectives and Limitations, *Open Waste Manag. J.* 10 (1) (2017) 13–22.

[20] Brazilian Institute of Geography and Statistics, Agriculture and Livestock Census 2017. (2018). [Online]. Available: <https://sidra.ibge.gov.br/home/lspa/brasil>. [Accessed: 25-Apr-

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457 2018].

[21] J. Dias, D. R.; Valencia, N. R.; Franco, D. A. Z.; Lopéz-Núñez, Management and utilization of wastes from coffee processing, *Cocoa coffee Ferment.*, no. Boca Raton: CRC Taylor & Francis. (2014) 376–382.

[22] P. S. Murthy and M. Madhava Naidu, Sustainable management of coffee industry by-products and value addition - A review, *Resour. Conserv. Recycl.* 66 (2012) 45–58.

[23] F. Passos, P. H. M. Cordeiro, B. E. L. Baeta, S. F. de Aquino, and S. I. Perez-Elvira, Anaerobic co-digestion of coffee husks and microalgal biomass after thermal hydrolysis, *Bioresour. Technol.* 253 (2018) 49–54.

[24] L. Wilson, G. R. John, C. F. Mhilo, W. Yang, and W. Blasiak, Coffee husks gasification using high temperature air/steam agent, *Fuel Process. Technol.*, 91 (10) (2010) 1330–1337.

[25] T. M. Ismail, M. Abd El-Salam, E. Monteiro, and A. Rouboa, Eulerian - Eulerian CFD model on fluidized bed gasifier using coffee husks as fuel, *Appl. Therm. Eng.* 106 (2016) 1391–1402.

[26] J. L. De Oliveira, J. N. Da Silva, E. Graciosa Pereira, D. Oliveira Filho, and D. Rizzo Carvalho, Characterization and mapping of waste from coffee and eucalyptus production in Brazil for thermochemical conversion of energy via gasification, *Renew. Sustain. Energy Rev.* 21 (2013) 52–58.

[27] C. A. García, Á. Peña, R. Betancourt, and C. A. Cardona, Energetic and environmental assessment of thermochemical and biochemical ways for producing energy from agricultural solid residues: Coffee Cut-Stems case, *J. Environ. Manage.* 216 (2017) 160–168.

[28] C. M. S. da Silva *et al.*, Biomass torrefaction for energy purposes – Definitions and an overview of challenges and opportunities in Brazil, *Renew. Sustain. Energy Rev.* 82 (2018) 2426–2432.

[29] J. O. Brito, F. G. Silva, M. M. Leão, and G. Almeida, Chemical composition changes in eucalyptus and pinus woods submitted to heat treatment, *Bioresour. Technol.* 99 (18)

- 1
2
3
4 485 (2008) 8545–8548.
5
6
7 486 [30] C. L. Mendoza Martinez *et al.*, Characterization of residual biomasses from the coffee
8
9 487 production chain and assessment the potential for energy purposes, *Biomass and*
10 488 *Bioenergy*, 120 (2019) 68–76.
11
12
13 489 [31] DIN, German Institute for Standardizatio: DIN EN ISO 14780:2017 Solid biofuels -
14
15 490 Sample preparation. 2017.
16
17 491 [32] DIN, German Institute for Standardization: DIN EN 14774-1 Solid biofuels -
18
19 492 Determination of moisture content, 2010.
20
21
22 493 [33] DIN, German Institute for Standardization: DIN EN 14775 - Solid biofuels -
23
24 494 Determination of ash content. 2012.
25
26 495 [34] DIN, German Institute for Standardization: DIN EN 15148 - Solid biofuels -
27
28 496 Determination of the content of volatile matter, 2010.
29
30
31 497 [35] DIN, German Institute for Standardization: DIN EN 15103 - Solid biofuels -
32 498 Determination of bulk density, 2010.
33
34
35 499 [36] DIN, German Institute for Standardization: DIN EN 14918 - Solid biofuels -
36
37 500 Determination of calorific value, 2014.
38
39 501 [37] B. R. Vital, Métodos de determinação da densidade da madeira, *Viçosa, MG:SIF*, 1984.
40
41
42 502 [38] T. de P. Protásio, I. C. N. Alves, P. F. Trugilho, V. O. Silva, and A. E. R. Baliza,
43
44 503 Compactação de biomassa vegetal visando à produção de biocombustíveis sólidos, *Pesqui.*
45 504 *Florest. Bras.* 31(68) (2011) 273–283.
46
47
48 505 [39] Soft, S, STATISTICA (data analysis software system), version 8.0, 2007.
49
50
51 506 [40] A. J. Regazzi and C. H. O. Silva, Testes para verificar a igualdade de parâmetros e a
52 507 identidade de modelos de regressão não-linear em dados de experimento com
53
54 508 delineamento em blocos casualizados, *Rev. Ceres.* 57 (3) (2010) 315–320.
55
56
57 509 [41] S. Mani, L. G. Tabil, and S. Sokhansanj, Effects of compressive force, particle size and
58 510 moisture content on mechanical properties of biomass pellets from grasses, *Biomass and*
59
60 511 *Bioenergy.* 30 (7) (2006) 648–654.
61
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65

[42] N. Kaliyan and R. Vance Morey, Factors affecting strength and durability of densified biomass products, *Biomass and Bioenergy*. 33 (3) (2009) 337–359.

[43] L. Guo, L. G. Tabil, D. Wang, and G. Wang, Influence of moisture content and hammer mill screen size on the physical quality of barley, oat, canola and wheat straw briquettes, *Biomass and Bioenergy*. 94 (2016) 201–208.

[44] S. Mani, L. G. Tabil, and S. Sokhansanj, Grinding performance and physical properties of wheat and barley straws, corn stover and switchgrass, *Biomass and Bioenergy*. 27 (4) (2004) 339–352.

[45] S. J. Mitchual, K. Frimpong-Mensah, and N. A. Darkwa, Effect of species, particle size and compacting pressure on relaxed density and compressive strength of fuel briquettes, *Int. J. Energy Environ. Eng.* 4 (1) (2013) 1–6.

[46] J. S. Tumuluru, C. T. Wright, J. R. Hess, and K. L. Kenney, A review of biomass densification systems to develop uniform feedstock commodities for bioenergy application, *Biofuels, Bioproducts and Biorefining*. 5 (6) (2011) 683–707.

[47] S. Mani, L. G. Tabil, and S. Sokhansanj, Specific energy requirement for compacting corn stover, *Bioresour. Technol.* 97 (12) (2006) 1420–1426.

[48] W. Quirino, Utilização energética de resíduos vegetais. 2002.

[49] P. D. Grover and S. K. Mishra, Biomass Briquetting: Technology and Practices, *Reg. Wood Energy Dev. Program. Asia*, (46) (1996) 1–48.

[50] Y. Li and H. Liu, High-pressure densification of wood residues to form an upgraded fuel, *Biomass and Bioenergy*, 19 (3) (2000) 177–186.

[51] I. Obernberger and G. Thek, Physical characterisation and chemical composition of densified biomass fuels with regard to their combustion behaviour, *Biomass and Bioenergy*. 27 (6) (2004) 653–669.

[52] M. Brožek, The Effect of Moisture of the Raw Material on the Properties Briquettes for Energy Use, *Acta Univ. Agric. Silvic. Mendelianae Brun.* 64 (2016) 1453-1458.

[53] E. R. K. Fernandes, C. Marangoni, O. Souza, and N. Sellin, Thermochemical

- 1
2
3
4 539 characterization of banana leaves as a potential energy source, *Energy Convers. Manag.*,
5
6 540 75 (2013) 603–608.
7
8
9 541 [54] R. García, C. Pizarro, A. Lavín, J. Bueno. Characterization of Spanish biomass wastes for
10 542 energy use, *Bioresource Technology*. 103 (1) (2012) 249-258.
11
12
13 543 [55] B. M. Jenkins, Fuel properties for biomass materials, *International symposium on*
14
15 544 *Application and Management of Energy in Agriculture: The Role of Biomass Fuels*. New
16 545 Delhi, 1990.
17
18
19 546 [56] S. Munir, S. S. Daood, W. Nimmo, A. M. Cunliffe, and B. M. Gibbs, Thermal analysis
20
21 547 and devolatilization kinetics of cotton stalk, sugar cane bagasse and shea meal under
22
23 548 nitrogen and air atmospheres, *Bioresour. Technol.* 100 (3) (2009) 1413–1418.
24
25 549 [57] L. Yanfen and M. Xiaoqian, Thermogravimetric analysis of the co-combustion of coal and
26
27 550 paper mill sludge, *Appl. Energy*. 87 (11) (2010) 3526–3532.
28
29
30 551 [58] Nogueira, L. A. H., Lora, E. E. S., Trossero, M. A., Frisk, T., *Dendroenergia:*
31 552 *fundamentos e aplicações*. National Electric Power Agency of Brazil, 2000.
32
33
34 553 [59] T. Raj *et al.*, Physical and chemical characterization of various indian agriculture residues
35
36 554 for biofuels production, *Energy and Fuels*. 29 (5) (2015) 3111–3118.
37
38 555 [60] I. Obernberger and G. Thek, *The pellet handbook: The production and thermal utilisation*
39 556 *of biomass pellets*. 2010.
40
41
42 557 [61] J. Diniz, A. D. L. Cardoso, J. A. Stahl, M. A. Villetti, and A. F. Martins, Poder Calorífico
43 558 da Casca de Arroz, Caroço de Pêssego, Serragem de Eucalipto e de seus Produtos de
44
45 559 Pirólise, *Ciência e Natura*. 26 (2) (2004) 25–32.
46
47
48
49 560 [62] S. Nanda, P. Mohanty, K. K. Pant, S. Naik, J. A. Kozinski, and A. K. Dalai,
50
51 561 Characterization of North American Lignocellulosic Biomass and Biochars in Terms of
52
53 562 their Candidacy for Alternate Renewable Fuels, *Bioenergy Res*. 6 (2) (2013) 663–677.
54
55 563 [63] V. C. Soares, M. L. Bianchi, P. F. Trugilh, J. Höfler, and A. J. Pereira, Análise das
56
57 564 propriedades da madeira e do carvão vegetal de híbridos de eucalipto em três idades,
58
59 565 *Cerne*. 21 (2) (2015) 191–197.
60
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62
63
64
65

[64] A. Demirbaş, Biomass resource facilities and biomass conversion processing for fuels and chemicals, *Energy Convers. Manag.* 42 (11) (2001) 1357–1378.

[65] N. V. Avelar, A. A. P. Rezende, A. de C. O. Carneiro, and C. M. Silva, Evaluation of briquettes made from textile industry solid waste, *Renew. Energy.* 91 (2016) 417–424.

[66] Rodrigues, V. A. J., Silva, C. M., Carneiro, A. C. O., Rezende, A. A. P., Santos, L. S., & Ikawa, G. A., The use of pulp mill solid wastes for energy production. Proceedings of the 3th International Symposium on Energy from Biomass and Waste. (2010) 8–11.

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Table 1. Particle size distribution of the lignocellulosic residues used in the production of briquettes.

Biomass material	Designation	Particle size [mm]		
		$\emptyset < 0.31$	$0.31 \leq \emptyset < 0.47$	$0.47 \leq \emptyset \leq 2$
Pine	Wood	60.3%	19.0%	20.7%
	Stem	51.2%	22.2%	26.6%
Coffee	Primary Branch	47.5%	21.4%	31.1%
	Secondary Branch	45.1%	16.6%	38.3%
	Parchment	21.9%	35.3%	42.8%

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Table 2. Chemical characterization of the lignocellulosic residues.

Parameter	Unit	Biomasses					
		PW	CS	PB	SB	MIX	CCP
MC	wt %	12.23 a	10.96 a	8.70 c	9.28 b	9.65 b	11.09 a
VM ^a	wt %	82.46 a	79.76 ab	80.67 a	76.50 bc	79.57 ab	73.80 c
FC ^a	wt %	16.79 b	18.09 ab	17.05 ab	19.36 ab	14.62 d	20.09 ab
AC ^a	wt %	0.75 d	2.15 c	2.27 c	4.14 b	2.63 c	5.91 a
HHV	MJ/kg	20.71 a	20.12 b	19.75 bc	19.72 c	19.86 bc	18.92 d

^adry basis; MC-moisture content; VM-volatile matter; FC-fixed carbon content; AC-ash content; HHV-higher heating value; PW-pinewood; CS-coffee stem; PB-primary branch; SB-secondary branch; MIX=CS+PB+SB; CCP-Coffee Cherry Parchment.

Averages along the rows followed by the same letter among biomasses do not differ by Tukey test at 5% of significance.

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Table 3. Compaction rate of the briquettes produced with studied biomasses.

PW (%)	Biomasses				
	CS	PB	SB	MIX	CCP
0	3.67	3.92	4.43	4.53	3.48
25	5.02	15.16	16.25	17.23	14.58
50	18.81	21.64	19.30	19.52	20.13
75	24.12	24.29	25.86	25.41	25.88
100	11.78	11.78	11.78	11.78	11.78

PW-pinewood; CS-coffee stem; PB-primary branch; SB-secondary branch; MIX=CS+PB+SB; CCP-Coffee Cherry Parchment

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Table 4. Covariance analysis for the properties measured in the briquettes.

VS	DF	SQ	MQ	F	P (>F)
Equilibrium moisture content					
IM	4	4	1	8.15	0.62E-04
Residual	18	2.21	0.12		
Energy density					
IM	4	1771328	442832	3.04	0.043
Residual	18	259174	143984		
Apparent density					
IM	4	23151	5788	6.60	1.88E-03
Residual	18	15784	877		
Maximum load					
IM	4	12001	3000	2.7035	0.06
Residual	18	19976	1110		

VS-Variation sources; DF-Degrees of freedom; SQ-Sum square; MQ-Mean square; F-F calculated statistics; p-statistical probability F tabulated; IM-Identity model.

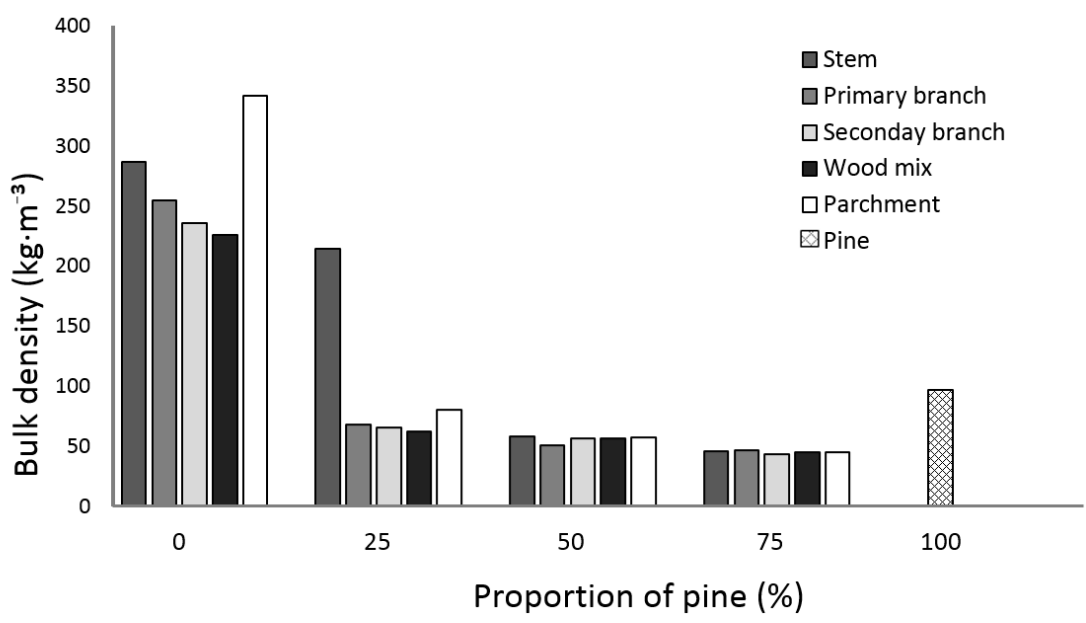
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Table 5. Adjusted equation for the physical – chemical properties of briquettes.

Property	Treatment	Adjusted Equation			R ²
		β_0	β_1	β_2	
Equilibrium moisture	CS-MIX model	2E-06	2.1E-03	9.65	0.99
	PB-SB model	9E-05	-1.3E-02	10.23	0.76
	CCP model	3E-05	-2.3E-02	11.84	0.99
Energy density	General model*	-1.9E-01	46.60	16835	0.99
	CCP model	- 1.8E-01	35.34	17995	0.93
Apparent density	General model*	-4.3E-03	1.5	1027	0.99
	CCP model	1E-05	- 4.4E-01	1185	0.85
Maximum load	General model	3.2E-02	2.5	139	0.99

*Adjusted equation for briquettes without presence of CCP in its composition; CS - Coffee Stem; PB - Primary Branch; SB - Secondary Branch; Mix=CS+PB+SB; CCP - Coffee Cherry Parchment. R² – Coefficient of determination. $\beta_0, \beta_1, \beta_2$ – Regression coefficients.

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Wood mix = stem + primary branch + secondary branch

Figure 1. Bulk density of studied biomasses (raw material).

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CS-coffee stem; PB-primary branch; SB-secondary branch; MIX=CS+PB+SB; CCP-Coffee Cherry Parchment.

Figure 2. Briquettes produced from coffee residues mixed with pinewood in different ratios.

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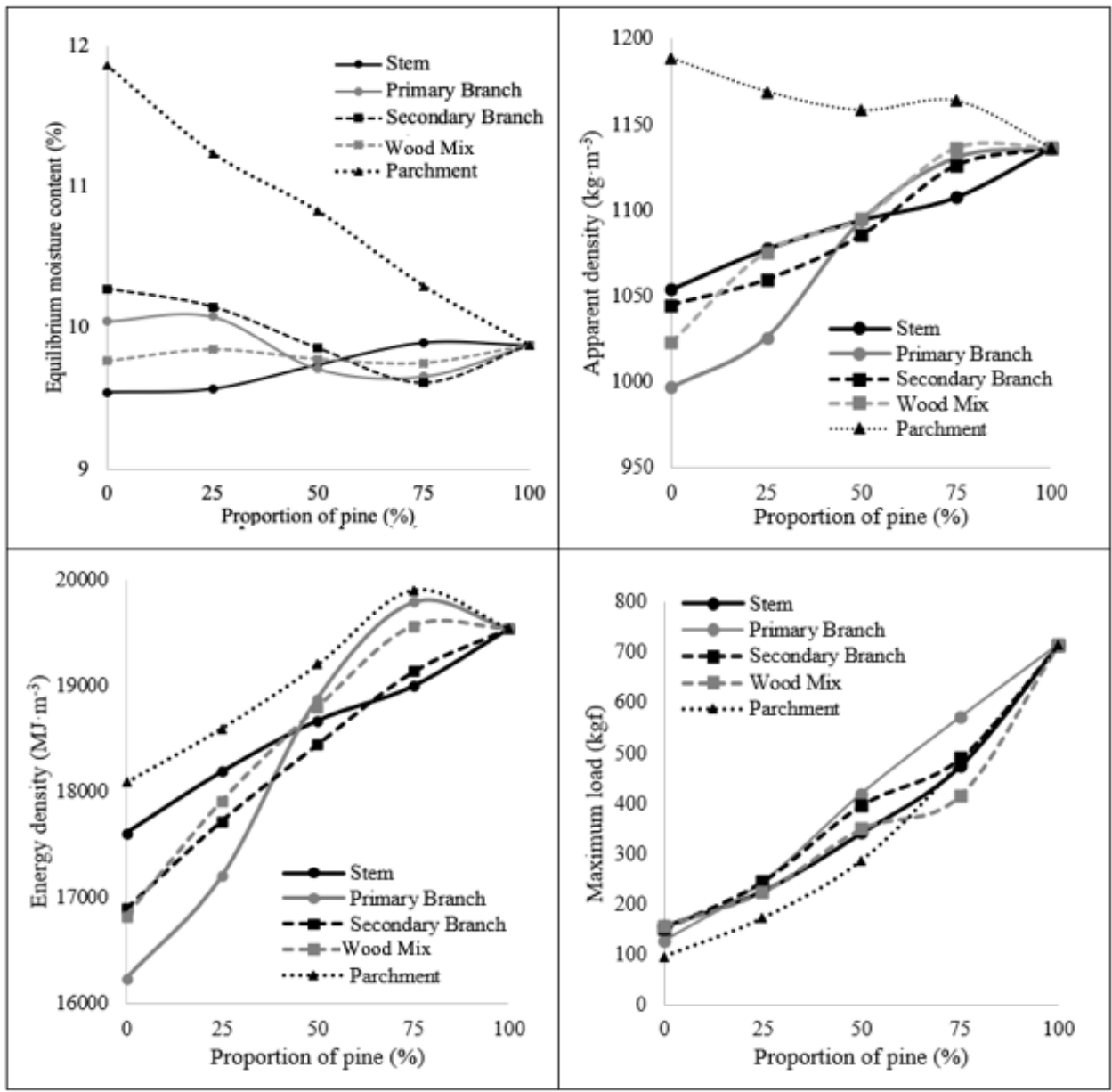


Figure 3. Properties of briquettes produced with the studied biomasses: equilibrium moisture content (upper-left), apparent density (upper-right), energy density (lower-left) and compressive strength (lower-right).

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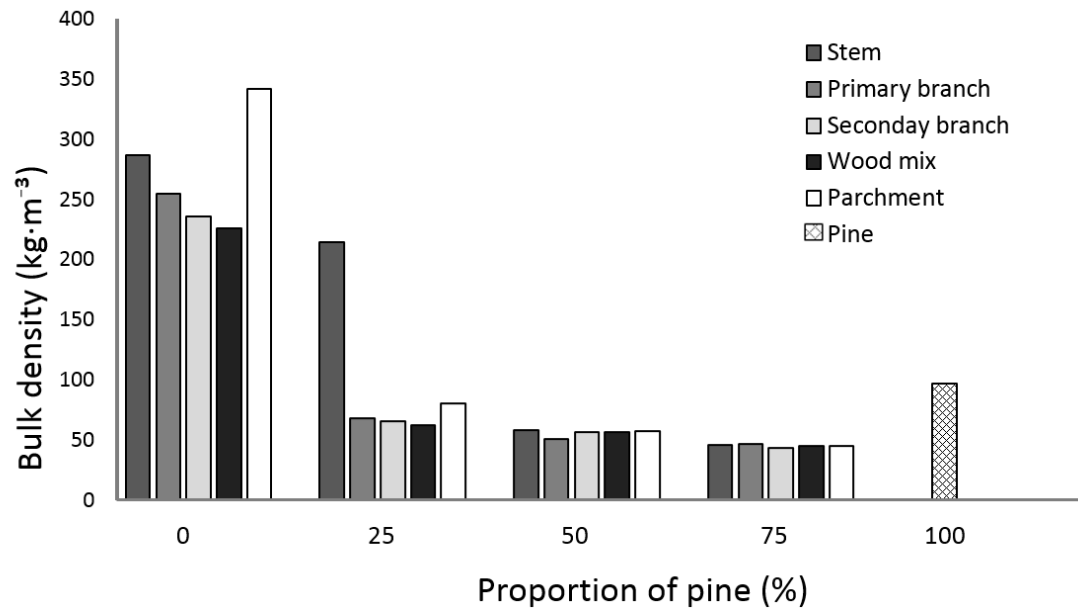
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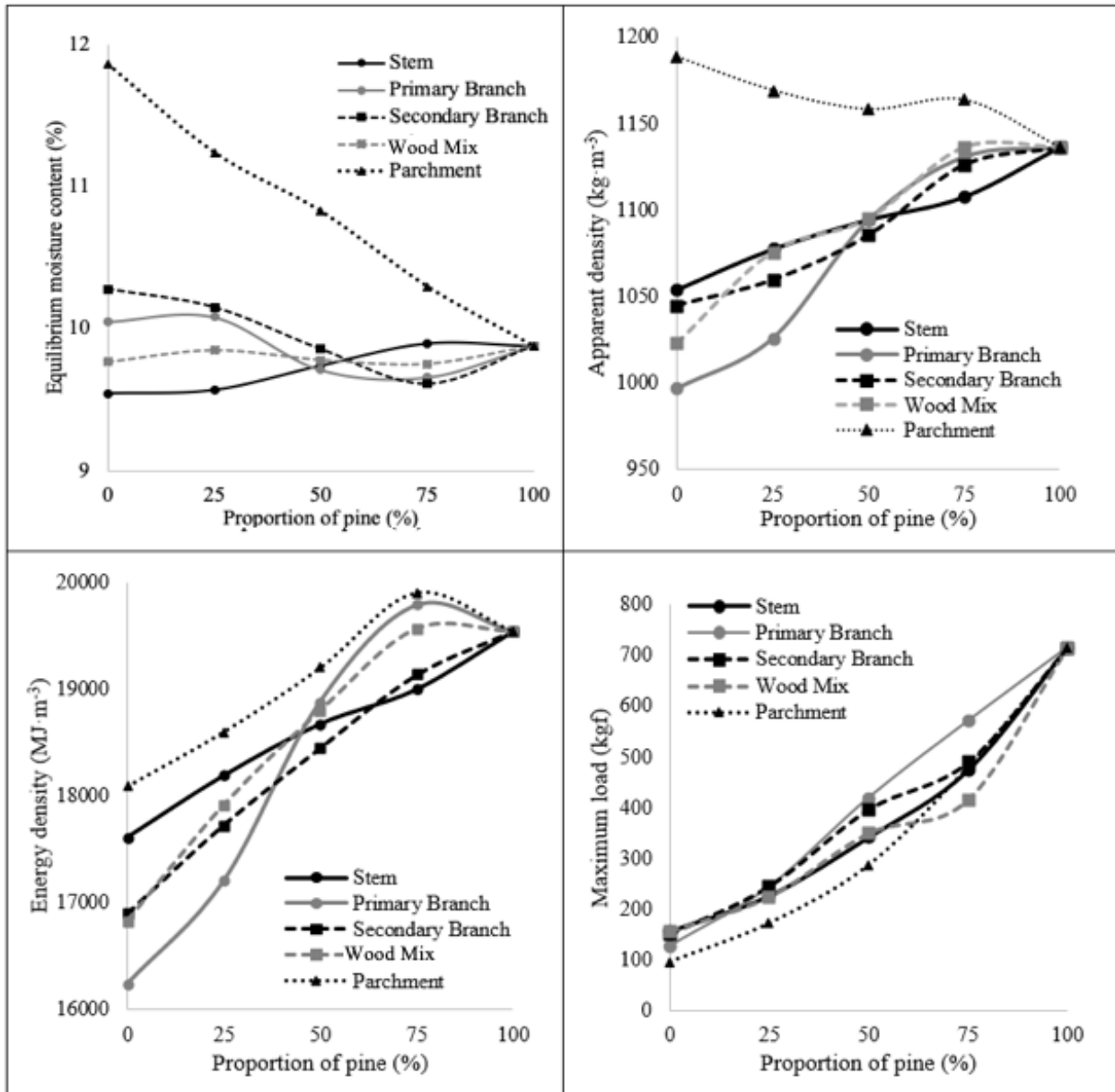


Figure 3. Properties of briquettes produced with the studied biomasses: equilibrium moisture content (upper-left), apparent density (upper-right), energy density (lower-left) and compressive strength (lower-right).